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INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

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(54) Title: METHODS OF PRESERVING PROKARYOTIC CELLS AND COMPOSITIONS OBTAINED THEREBY (57) Abstract <p>This invention provides methods of drying and stabilizing prokaryotic cells, and the compositions obtained thereby. The cells are first cultured or incubated under conditions sufficient to induce intracellular trehalose, suspended in a stabilizing solution and dried to form a solid glass. The resulting product is storage-stable at room temperature, showing little viability loss on storage.</p>		

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METHODS OF PRESERVING PROKARYOTIC CELLS AND COMPOSITIONS OBTAINED THEREBY

TECHNICAL FIELD

5 This invention relates to the field of preserving cells. More specifically, it relates to methods of drying and stabilizing prokaryotic cells and the compositions obtained thereby.

BACKGROUND ART

10 Live prokaryotic cells, particularly bacteria, are widely and increasingly used in important medical, agricultural and industrial applications. Agricultural, or environmental, applications include biopesticides and bioremediation. Medical applications include use of live bacteria in vaccines as well as production of pharmaceutical products and numerous industrial compositions. The use of live bacterial vaccines promises only to increase, given the dramatic rise in biotechnology as well as the intensive research into the treatment of infectious diseases over the past twenty years.

15 Bacterial cells must be able to be stored for significant periods of time while preserving their viability to be used effectively both in terms of desired results and cost. Storage viability has proven to be a major difficulty. Methods for preserving live prokaryotic cells suffer from several serious drawbacks, such as being energy-intensive and requiring cold storage. Furthermore, existing preservation methods fail to provide satisfactory viability upon storage, especially if cells are stored at ambient or higher temperature.

25 Freeze-drying is often used for preservation and storage of prokaryotic cells. However, it has the undesirable characteristics of significantly reducing viability as well as being time- and energy-intensive and thus expensive. Freeze-drying involves placing the cells in solution, freezing the solution, and exposing the frozen solid to a vacuum under conditions where it remains solid and the

water and any other volatile components are removed by sublimation. The resulting dried formulation comprises the prokaryotic cells.

In spite of the apparent ubiquity of freeze-drying, freeze-dried bacteria are unstable at ambient temperatures, thus necessitating storage by refrigeration. Even when refrigerated, however, the cells can quickly lose viability. Damage caused by this process may be circumvented, to a certain degree, by the use of excipients such as lyoprotectants. However, lyoprotectants may subsequently react with the dried cells, imposing inherent instability upon storage of the freeze-dried prokaryotic cells.

Other methods used to prepare dry, purportedly stable preparations of prokaryotic cells such as ambient temperature drying, spray drying, liquid formulations, and freezing of bacterial cultures with cryoprotectants also have drawbacks. For a general review on desiccation tolerance of prokaryotes, see Potts (1994) *Micro. Rev.* 58:755-805. Ambient temperature drying techniques eliminate the freezing step and associated freeze-damage to the substance, and these techniques are more rapid and energy-efficient in the removal of water. Crowe *et al.* (1990) *Cryobiol.* 27:219-231. However, ambient temperature drying often yields unsatisfactory viability. Spray drying results in limited storage time and reduced viability, even when stabilizing excipients are used. For a general review, see Lievense and van't Reit (1994) *Adv. Biochem. Eng. Biotechnol.* 51:45-63; 72-89. Liquid formulations may provide only short-term stabilization and require refrigeration. Freezing bacterial cultures results in substantial damage to the bacterial cell wall and loss of viability which is only reduced but not eliminated by the use of cryoprotectants. Moreover, these frozen cultures also need to be stored refrigerated.

Trehalose, (α -D-glucopyranosyl- α -D-glucopyranoside), is a naturally occurring, non-reducing disaccharide which was initially found to be associated with the prevention of desiccation damage in certain plants and animals which can dry out without damage and can revive when rehydrated. Trehalose has been shown to be useful in preventing denaturation of proteins, viruses and foodstuffs

during desiccation. See U.S. Patent Nos. 4,891,319; 5,149,653; 5,026,566; Blakeley et al. (1990) *Lancet* 336:854-855; Roser (July 1991) *Trends in Food Sci. and Tech.* 10:166-169; Colaco et al. (1992) *Biotechnol. Internat.* 1:345-350; Roser (1991) *BioPharm.* 4:47-53; Colaco et al. (1992) *Bio/Tech.* 10:1007-1011; and Roser et al. (May 1993) *New Scientist*, pp. 25-28. Trehalose dihydrate is available commercially in good manufacturing process (GMP) grade crystalline formulations. A method of making trehalose from starch is described in EP patent publication No. 639 645 A1. This method involves a two step enzymatic bioconversion of starch to yield a trehalose syrup from which the sugar is recovered by crystallisation.

Bacteria are able to counteract osmotic shock by accumulating and/or synthesizing potassium with a few types of organic molecules, including some sugars. Osmoregulation in bacteria such as *Escherichia coli* in glucose-mineral medium without any osmoprotective compounds involves the endogenous production of trehalose. Larsen et al. (1987) *Arch. Microbiol.* 147:1-7; Dinnbier et al. (1988) *Arch. Microbiol.* 150:348-357; Giaever et al. (1988) *J. Bacteriol.* 170:2841-2849; and Welsh et al. (1991) *J. Gen. Microbiol.* 137:745-750.

One method of preserving prokaryotic cells is freeze-drying in the presence of trehalose. See, e.g., Israeli et al. (1993) *Cryobiol.* 30:519-523. However, this method provides unsatisfactory viability. Israeli et al. freeze dried *E. coli* in the presence of 100 mM trehalose but reported survival data for only four days after exposure of the dried samples to air at 21°C. A later study tested survival rates of *E. coli* and *Bacillus fluoringiensis* freeze-dried in the presence of trehalose. Leslie et al. (1995) *Appl. Env. Microbiol.* 61:3592-3597. Survival data were reported only for 4 days after exposure of the dried samples to air.

Another study comparing freeze-dried to air-dried (sealed under nitrogen) *E. coli* in the presence of trehalose reported survival rates of about 10^7 to over 10^{10} colony forming units (CFU) per ml for cells stored for 25 weeks, but the cells were stored at 4°C. Louis et al. (1994) *Appl. Microbiol. Biotechnol.* 41:684-688.

In view of increasing applications for viable bacteria and the existing problems regarding maintaining bacterial viability during storage, there is a pressing need for a method to inexpensively dry and stabilize prokaryotic cells. It is especially desirable to develop methods that would allow storage of dried prokaryotic cells at ambient temperature, i.e., not requiring refrigeration. The methods described herein address this need by providing dry, remarkably storage-stable, prokaryotic cells that retain viability without the need for refrigeration.

All references cited herein are hereby incorporated herein by reference in their entirety.

SUMMARY OF THE INVENTION

The present invention encompasses methods of producing dried, stabilized prokaryotic cells. The invention also includes compositions produced by these methods, as well as methods of reconstituting the prokaryotic cells.

Accordingly, in one aspect, the invention provides methods of preserving prokaryotic cells, comprising culturing the prokaryotic cells under conditions which increase intracellular trehalose concentration to an amount effective to increase storage stability, mixing the prokaryotic cells with a drying solution which comprises a stabilizing agent such as trehalose, and drying the prokaryotic cells such that a glass is produced having less than about 5% residual moisture.

BRIEF DESCRIPTION OF THE DRAWINGS

Figure 1 shows the alignment of trehalose synthase amino acid sequences encoded by genes from a variety of organisms: 1. *Kluyveromyces lactis*; 2. *Saccharomyces cerevisiae*; 3. *Aspergillus niger*; 4. *Schizosaccharomyces pombe*; 5. *Mycobacterium leprae* and 6. *E. coli* (SEQ. ID NOS: 1-6, respectively).

Figure 2 is a half-tone reproduction of a Southern blot testing for the presence of trehalose synthase genes in *E. coli* and *Salmonella*. The horizontal lines on the left represent molecular weight markers (λ Hind III) of 23, 9.3, 6.6, 4.4, 2.3, 2.0 and 0.56 kb, respectively.

Figure 3 is a graph depicting stability of *E. coli* NCIMB 9484 after storage at 37°C. The circles indicate intracellular trehalose induction and the triangles represent no trehalose induction.

Figure 4 is a graph depicting the relationship between T_g and residual moisture in a formulation of 45% trehalose and 1.5% Kollidon 90.

Figure 5 is a graph depicting the relationship between residual moisture and length of drying time in a formulation of 45% trehalose and 0.1% CMC. The FTS drying protocol was 30 mT ST 40°C (x hrs).

Figures 6A and 6B are graphs depicting the effect of a high osmolarity condition (0.5M NaCl) on intracellular trehalose concentration. Figure 6A shows the accumulation of intracellular trehalose concentration and growth curve for *E. coli* grown at 37°C in Evans medium and 0.5 M NaCl. Figure 6B shows accumulation of intracellular trehalose concentration and growth curve at 37°C for *E. coli* grown at 37°C in Evans medium lacking NaCl. In both A and B, the circles represent induced trehalose concentration and the squares represent cell growth (absorbance) measured at 600 nm.

Figure 7 is a reproduction of a series of tracings from a HPLC analysis of intracellular trehalose concentration in *Salmonella* before and after trehalose induction by osmotic shock.

Figure 8 is a graph depicting the relationship between cell viability and length of drying time in a formulation of 45% trehalose and 0.1% CMC. The FTS drying protocol was 30 mT ST 40°C (x hrs).

Figure 9 is a graph depicting intracellular trehalose (●) and protein (v) concentration during growth of *S. typhimurium* at 37°C.

Figure 10 is a graph depicting the percent recovery of trehalose induced (●) and non-induced (σ) *S. typhimurium* 1344 after storage at 37°C.

MODES FOR CARRYING OUT THE INVENTION

We have found that prokaryotic cells can be dried and stabilized by inducing intracellular trehalose production to an amount effective to increase storage stability and drying the cells in the presence of a stabilizing agent. The methods for stabilizing prokaryotic cells described herein can be used for producing dried, stable bacteria useful for pharmacological treatment, prophylaxis, agricultural and industrial applications.

Prokaryotic cells obtained by the methods disclosed herein are remarkably stable: bacteria stabilized by these methods retain high viability even after storage at ambient or above ambient temperatures. Bacteria dried under these conditions retain about 50-80% viability upon drying. Furthermore, bacteria stabilized by these methods show less than 10% loss of viability on storage even after being stored at temperatures up to at least 37°C for as long as six weeks. This degree of stabilization during drying and storage is significantly greater than previously reported using other methods. The stabilized cells can be stored at room temperature and thus do not require refrigeration. Depending on the conditions, drying can generally be accomplished within 24 hours which provides energy and cost savings as well as increased viability.

The methods and compositions of the invention facilitate the development of many needed, useful products, including, but not limited to: (i) live bacterial vaccines in a dry stable form; (ii) live bacterial nutraceuticals in a dry stable form; (iii) other live bacterial pharmaceutical products in a dry stable form, e.g., for treatment of vaginal or urinary tract infections; (iv) live bacterial starter cultures in a dry stable form for commercial products such as for the dairy industry; (v) live bacteria in a dry stable form for agricultural, ecological or bioremedial use, such as pesticides; and (vi) live bacterial cultures in a dry stable form for the biotechnology industry.

As used herein, "prokaryotic cells" are cells that exhibit characteristics of prokaryotes, which is a term well known in the art. Prokaryotes are typically unicellular organisms and lack organelles (such as mitochondria, chloroplasts, and

Golgi apparatus), a cytoskeleton, and a discrete nucleus. Examples of prokaryotic cells include bacteria, such as eubacteria, cyanobacteria and prochlorophytes; archaeobacteria; and other microorganisms such as rickettsias, mycoplasmas, spiroplasmas, and chlamydiae. For purposes of this invention, prokaryotes are capable of synthesizing trehalose. This ability can be native or conferred by recombinant techniques. The ability to synthesize trehalose can be determined by measuring intracellular trehalose concentration, which is described below. Preferably, the prokaryotic cells are bacteria.

The stabilizing agents are preferably carbohydrates. "Carbohydrates" include, but are not limited to, monosaccharides, disaccharides, trisaccharides, oligosaccharides and their corresponding sugar alcohols, polyhydroxyl compounds such as carbohydrate derivatives and chemically modified carbohydrates, hydroxyethyl starch and sugar copolymers. Both natural and synthetic carbohydrates are suitable for use herein. Synthetic carbohydrates include, but are not limited to, those which have the glycosidic bond replaced by a thiol or carbon bond. Both D and L forms of the carbohydrates may be used. For purposes of this invention, the carbohydrate is preferably non-reducing. Preferably, the non-reducing carbohydrate is trehalose. Other examples of preferred non-reducing carbohydrates are provided below.

Conditions that "increase intracellular trehalose concentration" are conditions that initiate, encourage, allow, and/or increase the rate of synthesis of trehalose within the cell(s), and/or increase the amount of trehalose within the cell(s) when compared to growing or incubating the cell(s) without these conditions. Conditions (including preferred conditions) that stimulate production of intracellular production of trehalose are discussed in detail below. Examples of these conditions include, but are not limited to, growing the cell(s) under stressful conditions such as osmotic shock, i.e., high salt conditions. Conditions that stimulate production of intracellular trehalose can also be effected by, for example, inhibiting the rate of degradation of trehalose, expressing recombinant genes and inducing uptake of exogenous trehalose.

"Ambient" is a term of art referring to the atmospheric pressure or humidity or temperature of the room in which the methods described are being performed. Ambient temperature is also referred to as room temperature and is generally from about 15-25°C.

5 "Residual moisture" is the amount of water remaining (expressed in weight percent) after drying prokaryotic cells by the methods described herein. Residual moisture can be measured by Karl/Fischer Coulometer, as discussed in more detail below.

10 "Glass" is a term well understood in the art, especially as applied to carbohydrate glasses. For purposes of this invention, "glass" refers to a non-crystalline, vitreous, solid physical state achieved upon sufficient loss of water.

 As used herein, "foamed glass matrix" (FGM) refers to a carbohydrate-containing glass that contains bubbles dispersed in the glass, resulting in a foam. For purposes of this invention, a foamed glass matrix contains less than about 5% residual moisture, preferably less than about 4% residual moisture, more
15 preferably less than about 2% residual moisture.

 "High osmolarity" refers to excessive solute concentration in growth media. "Excessive" solute concentration means that solute concentration (generally salts) is above the level at which a cell exists and/or grows in its native
20 environment.

 "Viability" is a term well understood in the art, and is consonantly used herein to mean manifestations of a functioning living organism, such as metabolism and cell division. Methods to measure viability are known in the art and are described herein.

25 The present invention encompasses methods of producing stabilized prokaryotic cells and the cells produced thereby. These methods comprise the steps of increasing intracellular trehalose, preferably by culturing or incubating the prokaryotic cells under conditions that increase intracellular trehalose concentration to an amount effective to increase storage stability; mixing the
30 prokaryotic cells with a drying solution which contains a stabilizing agent.

preferably a non-reducing carbohydrate such as trehalose; and drying the resulting mixture such that a glass is produced having less than about 5% residual moisture.

Growing prokaryotic cells to increase intracellular trehalose concentration. To practice the methods of this invention, prokaryotic cells can be grown under conditions that increase intracellular trehalose concentration. Intracellular trehalose can be measured using standard methods in the art as described below. Any prokaryotic cell, particularly bacteria, containing trehalose synthase genes, whether endogenous or recombinant, should be capable of producing intracellular trehalose.

Many types of prokaryotic cells are known to synthesize trehalose. Examples of bacteria that contain the trehalose synthase gene include, but are not limited to, Enterobacteriaceae, such as *Salmonella* and *Escherichia* (e.g., *S. typhimurium* and *E. coli*); halophilic and halotolerant bacteria, such as *Ectothiorhodospira* (e.g., *E. halochloris*); micrococcaceae, such as *Micrococcus* (e.g., *M. luteus*); *Rhizobium* species such as *R. japonicum* and *R. leguminosarum* bv *phaseoli*; *Cyanobacteria* and *Mycobacteria* species such as *M. tuberculosis*, *M. bovis*, and *M. smegmatis*. An alignment of trehalose synthases encoded by genes from a variety of organisms is shown in Figure 1. Several other bacteria have been shown to have trehalose synthase genes all of which are highly homologous to the *E. coli* gene. These bacteria include *Pseudomonas putidae* and *Aeromonas salmonicida*.

Determining whether a particular bacteria species contains trehalose synthase gene(s) can be accomplished by, for example, searching available nucleic acid (and/or protein) databases for the presence of sequences that encode (or that correspond to) consensus regions of the amino acid sequence for trehalose synthase genes. Bacteria have two genes involved in trehalose synthesis (i.e., T-Phosphate synthase and T-6-P phosphatase), whereas yeast have at least three genes. Generally, searching with probes specific for the yeast genes also identifies the bacterial genes, albeit with lower homology scores. Amino acid sequence alignments of trehalose synthase show homology between bacteria,

yeast and fungi and more specific search and screening probes can be determined from these alignments (Fig. 1). Alternatively, Southern blots can be produced of genomic DNA from a test cell probed with DNA encoding all or a functional portion of trehalose synthase gene. Figure 2 shows a Southern blot of the trehalose synthase genes of *E. coli*, and two strains of *Salmonella*.

Increases in intracellular trehalose can be obtained by culturing the cells under stressful conditions, e.g., osmotic shock, heat or oxygen limitation (shock), carbon/nitrogen starvation, or any combination of the above. Alternatively, use of inhibitors of enzyme(s) involved in trehalose degradation (i.e., trehalase), such as validomycin, also results in accumulation of intracellular trehalose. Suitable conditions can be determined empirically and are well within the skill of one in the art. While not wishing to be bound to a particular theory, induction of trehalose production under stressful conditions may trigger synthesis or accumulation of other molecules beneficial for preservation, such as betaine and chaperonins.

For bacteria, particularly *Escherichia*, trehalose production can be stimulated by growing the cell(s) in conditions of high osmolarity, i.e., solute (generally salt) concentrations sufficient to stimulate trehalose production. Thus, the invention encompasses culturing prokaryotic cells in osmolarity of at least about 350 mOsmoles to about 1.5 Osmoles, preferably at least about 400 mOsmoles to 1 Osmole, more preferably 250 mOsmoles to 500 mOsmoles. The invention also encompasses culturing prokaryotic cells in osmolarity of at least about 300 mOsmoles, preferably at least about 400 mOsmoles, more preferably at least about 500 mOsmoles. Generally, a minimum salt concentration of about 200 mOsmoles is required but an effective concentration can be derived empirically. A single salt can be sufficient to stimulate trehalose production, for example, 200 mM NaCl. KCl and CaCl₂ also stimulate intracellular trehalose production, indicating that intracellular trehalose production is not dependent on the action used or the concentration of chloride in the growth medium. When

(NH₄)₂SO₄ is used, however, only about one half of the amount of trehalose is produced compared to that produced in the presence of KCl, NaCl and CaCl₂. A combination of salts can also be used. In addition, when used to increase the osmolarity of the medium, a non-penetrant solute such as sorbitol and/or glucose can contribute to the stimulation of trehalose accumulation.

Examples of salts that can be used to increase the osmolarity include, but are not limited to, sodium phosphate (Na₂PO₄); potassium phosphate (KH₂PO₄); ammonium chloride (NH₄Cl); sodium chloride (NaCl); magnesium sulfate (MgSO₄); calcium chloride (CaCl₂); thiamine hydrochloride or any combination thereof. In a preferred embodiment, minimal medium contains about 0.5 M salt. Even more preferably, the 0.5 M salt is composed of the following: Na₂HPO₄, 6 g/l; KH₂PO₄, 3 g/l; NH₄Cl, 0.267 g/l; NaCl, 29.22 g/l; 1 M MgSO₄, 1 ml/l; 0.1 M CaCl₂ (1 ml/l); thiamine HCl, 1 ml/l; with glucose at final concentration of 2.5% w/v. Sufficient glucose should be available for a carbon source and trehalose production. Determining sufficient glucose concentrations can be determined empirically and is well within the skill of one in the art.

The salt concentration (i.e., osmolarity) required to stimulate and/or induce trehalose production will depend upon the genus, species, and/or strain of the prokaryotic cell used. Preferably, cell(s) are grown in a minimal medium containing salt. Commercially available minimal medium is supplemented with desired salts and/or other solutes, although minimal medium is not essential and defined media can also be used. The time required to initiate and achieve the desired level of intracellular trehalose concentration will vary depending on the level of osmolarity as well as the genus, species and/or strain of prokaryotic cell used and can be determined empirically. Trehalose synthesis will generally begin within an hour of placing cells in condition designed to stimulate trehalose production. Generally, in *E. coli* the amount of intracellular trehalose reaches a maximum at about 15 to 20 hours after placing cells in conditions that stimulate trehalose production.

To induce intracellular trehalose production by osmotic shock, the total concentration of salt(s) in the medium should be at least about 0.2 M, preferably at least about 0.4 M, more preferably at least about 0.5 M. In the case of *E. coli*, the total concentration of salt(s) should not exceed 0.6 M. At about 0.6 M or
5 above, intracellular trehalose production declines in *E. coli*. The salt concentration required for the desired result may vary depending on the general/species/strain used, and can be determined empirically.

Intracellular trehalose can also be increased using recombinant methods which are well known in the art. For instance, prokaryotic cells can be
10 transfected with a DNA plasmid comprising a DNA sequence encoding an appropriate trehalose synthase gene. Suitable genes are available from a wide variety of resources as indicated by the number of genes depicted in Figure 1 and other genes recently identified. The gene in turn is operatively linked to a suitable promoter, which can be constitutive or inducible. Recombinant methods
15 are described in a variety of references, such as "Molecular Cloning: A Laboratory Manual," second edition (Sambrook *et al.*, 1989).

Intracellular trehalose can be measured by using assays known in the art, such as by high pressure liquid chromatography (HPLC), coupled with electro-chemical detection and glucose assay (Trinder assay using trehalase) for
20 quantitative enzymatic determination of trehalose. Thin layer chromatography can be used as a qualitative method for the separation of different carbohydrates. Refractive index detection provides another means of detecting sugars quantitatively.

In measuring trehalose by HPLC, cells are disrupted and intracellular
25 trehalose preferentially solubilized in 70% ethanol, followed by removing triglycerides by chloroform extraction. Intracellular trehalose concentration is determined by multiplying trehalose concentration (as determined by a standard curve) by the fraction of final volume of supernatant divided by pellet volume. A more detailed description of this assay is provided in Example 1.

Preferably, the concentration of intracellular trehalose is at least about 50 mM; more preferably, at least about 100 mM; more preferably, at least about 150 mM; more preferably, at least about 200 mM; more preferably, at least about 250 mM; and even more preferably, at least about 300 mM. We have found that stability of bacteria decreases markedly using the methods described herein if the intracellular trehalose concentration is below about 30 mM. Thus, the invention encompasses culturing the prokaryotic cells under conditions that stimulate intracellular production of trehalose, wherein intracellular concentration of trehalose reaches at least about 30 mM, preferably at least about 50 mM, preferably at least about 100 mM, more preferably at least about 150 mM, more preferably at least about 200 mM, more preferably at least about 250 mM, and even more preferably at least about 300 mM.

The time required for stimulating intracellular trehalose production depends, inter alia, on the nature of the prokaryotic cells (including genus, species, and/or strain) and the conditions under which trehalose induction occurs (i.e., whether by osmotic shock, oxygen deprivation, etc.). For trehalose induction by osmotic shock, the time required for maximum concentration of intracellular trehalose in turn depends on the degree of osmolarity as well as the particular salts used. For example, in *E. coli*, ammonium sulfate ((NH₄)₂SO₄) stimulates about half the amount of intracellular trehalose concentration as NaCl, CaCl₂ or KCl. For *E. coli* in 0.5 M salt minimal media, maximum intracellular trehalose concentration occurs within about 10–17 hours, with significant induction by 17 hours after osmotic shock (Example 1; Figure 6).

As is readily apparent to those skilled in the art, achieving a desired intracellular trehalose concentration can also be effected by other means such as introducing trehalose into the cell(s). This can be accomplished, for example, by culturing cells in the presence of trehalose while subjecting the cell(s) to conditions that permeabilize the cell wall and membrane. Examples of such conditions include, but are not limited to, conditions that effect membrane phase transition (such as cycles of cooling and warming or osmotic shock) and

electroporation. The intracellular trehalose concentration can be determined for these conditions as described above. Conditions that effect membrane phase transition especially apply to Gram negative bacteria.

Accordingly, one embodiment of the present invention is a method of preserving prokaryotic cells comprising the steps of culturing the prokaryotic cells under conditions that increase intracellular trehalose concentration to a level effective to increase storage stability in the methods described herein, mixing the prokaryotic cells with a drying solution which contains a stabilizing agent, and drying the prokaryotic cells such that a glass is produced having less than about 5% residual moisture.

Mixing the prokaryotic cells with drying solution. After intracellular trehalose is increased to the desired degree, the prokaryotic cells are harvested by, for instance, centrifugation and resuspended in a drying solution containing a stabilizing agent, preferably a non-reducing carbohydrate such as trehalose.

Particularly preferred non-reducing carbohydrates are trehalose, maltitol (4-O- β -D-glucopyranosyl-D-glucitol), lactitol (4-O- β -D-galactopyranosyl-D-glucitol), palatinit [a mixture of GPS (α -D-glucopyranosyl-1 \rightarrow 6-sorbitol) and GPM (α -D-glucopyranosyl-1 \rightarrow 6-mannitol)], and its individual sugar alcohol components GPS and GPM and hydrogenated maltooligosaccharides and maltooligosaccharides.

In addition to trehalose, suitable stabilizing agents include, but are not limited to, non-reducing glycosides of polyhydroxy compounds selected from sugar alcohols and other straight chain polyalcohols. Other useful stabilizing agents include neotrehalose, lactoneotrehalose, galactosyl-trehalose, sucrose, lactosucrose, raffinose, stachyose and melezitose. Carbohydrates with mild reducing activity, such as maltohexose, maltoheptulose, Sepharose and Dextran, can also be used with Maillard reaction inhibitors as described in patent application PCT/GB95/01967. Maillard reaction inhibitors can also be used to improve the performance of unstable reducing carbohydrates such as sucrose.

The concentration of non-reducing carbohydrate(s) in the drying solution will depend on several variables, most particularly the genus, species, and/or strain of prokaryotic cell that is being stabilized and the method of drying. For *E. coli*, the non-reducing carbohydrate (trehalose) concentration is preferably at least about 25%, more preferably at least about 35%, even more preferably at least about 45% (w/v). Preferably, the carbohydrate concentration should be less than about 50%, as higher concentrations may interfere with effective drying.

The solvent(s) that forms the basis for the drying solution can be any of a number of substances, provided it does not significantly affect cell viability.

Preferably, the solvent is aqueous.

The drying solution can optionally contain additives that contribute to overall stability of the prokaryotic cells. Generally, preferred additives increase the viscosity of the drying solution, which in turn enhances the drying process by more efficient foam production with higher T_g s. Examples of additives include, but are not limited to, polyvinylpyrrolidone (Kollidon Series: 12, 17, 25, 30, 90; BASF), carboxymethyl cellulose (Blanose HF; Aqualon) hydroxypropyl cellulose and hydroxyethyl starch (HES; MW 200,000). Preferably, Kollidon 90 is present in the drying solution at a concentration of about 1.5%. Preferably, the concentration of carboxymethyl cellulose is about 0.1%. Particularly preferred is a drying solution containing about 45% trehalose and either about 1.5% Kollidon 90 or about 0.1% carboxymethyl cellulose. Other additives that can be used include volatile salts, which contribute to effective drying (via foam formation). Examples of volatile salts include, but are not limited to, ammonium bicarbonate, ammonium chloride, ammonium acetate and ammonium sulfate. However, when using these salts, it is possible that more effective drying may be counteracted by lower viability due to pH and salt-specific effects.

The volume of the drying solution added to the prokaryotic cells, and thus the density of the prokaryotic cells in the drying solution, can vary. However, too low a cell density proportionately increases the drying time per cell; too high a density may adversely affect rapidity and/or efficiency of foam formation and

thus drying. Moreover, too high a cell density could result in higher concentration of anti-foaming agents produced by the cells. Preferably, the cell density is about 4 to 8×10^9 cells (CFU) per ml. although densities as high as 2×10^{10} cells per ml have been used with success. Generally, the volume of drying solution is significantly less than the volume of culture medium used for increasing intracellular trehalose concentration. The optional volume will vary somewhat on the types of cells and solutes and can be readily determined empirically.

Drying the prokaryotic cells. Upon suspending in the drying solution, the prokaryotic cells are then dried such that a glass is formed. Drying can be effected using methods known in the art, including, but not limited to, air (i.e., ambient temperature) drying, spray drying, and freeze drying. As used herein, the glass containing the dried prokaryotic cells preferably has a residual moisture content less than about 5%.

Drying is preferably performed at pressure less than ambient (i.e., vacuum). Preferably, the pressure is about 0.1 to 0.075 Torr/mm Hg. More preferably, the pressure is about 0.075 to 0.05 Torr/mm Hg. Most preferably, the pressure is about 0.05 to 0.03 Torr/mm Hg and external temperature is about 40°C.

Preferably, drying occurs above freezing temperatures and under a vacuum such that a foamed glass matrix (FGM) is formed. PCT/GB96/0136. Vacuum drying under freezing conditions will lead to lower viability. For creation of a vacuum, any vacuum drier with a control, preferably programmable control, of the vacuum pressure and external temperature can be used. As an example, a pump is capable of providing a vacuum of 0.01 Torr/mm Hg and evacuating the product chamber down to 0.2-0.01 Torr/mm Hg in 15-20 minutes. The machines used in the present work were the FTS Systems Inc. (Stone Ridge, New York) Model TDS 0007-A with a VP-62P vacuum pump and a FD-0005-A

condenser module or the Labconco, Inc. (Kansas City) Model No. 77560 with a Lyph-Lock 12 condenser unit and an Edwards E2M8 two-stage vacuum pump.

Reduction of the external pressure has at least two desirable effects. First, it reduces the vapor pressure of the solvent in the gas phase, thus accelerating evaporation and drying. The increased rate of evaporation causes evaporative cooling unless external heat is applied to replace the latent heat of evaporation. Under vacuum, the rate of drying is limited by this energy input. Thus, the effect of increasing the external temperature is, surprisingly, to accelerate the rate of drying and not to increase the sample temperature. The second effect of reduced external pressure is to drastically lower the boiling point of the sample. Boiling can therefore be conducted by a very modest rise in sample temperature which does not have a deleterious effect on the product.

Preferably, drying occurs in two stages: first, holding external temperature constant for a period of time; and second, increasing the external temperature until drying is complete. The temperature can be increased gradually, for example, 10 degrees over an hour, or, more preferably the temperature can be increased in equal increments, with each increment held constant for a period of time. In one embodiment, the temperature is maintained at about 40°C for about 16 hours, followed by gradually increasing the temperature to about 80°C over about the next 4 hours.

In a preferred embodiment, the prokaryotic cells are dried as follows: the pressure is adjusted to 30 mT, with initial shelf temperature of 40°C for 16 hours; followed by incrementally increasing the shelf temperature to 80°C at a rate of 2.5°C per minute in increments of 2°C, while holding each increment for about 12 minutes. Following this protocol, foaming typically occurs within 60 minutes of the initiation of drying, and the drying procedure is completed within 24 hours without substantially compromising viability. Example 6 provides a protocol.

FGMs are also formed by evaporating bulk solvent from the drying solution to obtain a syrup, exposing the syrup to a pressure and temperature sufficient to cause boiling or foaming of the syrup, and removing moisture so that

residual moisture does not exceed about 4%, preferably about 3%, more preferably about 2.5%.

5 In the primary drying step, the solvent is evaporated to obtain a syrup. Typically, a "syrup" is defined as a solution with a viscosity in the region of 10^6 - 10^7 Pascal seconds. The syrup is not defined as a fixed concentration, but is a result of the bulk of the solvent evaporating from the mixture. Typically, a syrup is a viscous mixture containing the glass matrix-forming material and/or additives and/or prokaryotic cells, in a significantly higher concentration than that of the initial mixture. Typically, the evaporation step is conducted under conditions
10 sufficient to remove about 20% to 90% of the solvent to obtain a syrup. The viscosity of the syrup is preferably such that when the syrup boils, evaporation from the increased surface area, provided by extensive bubble formation, results in its vitrification.

15 Under the vacuum, rapid drying continues until the viscosity of the sample begins to increase. At this point, the reduced mobility of water molecules through the viscous syrup reduces the rate of evaporative cooling and the sample temperature rises until it reaches the boiling point at the reduced pressure. On boiling, a large increase in the area of the liquid/gas interface occurs due to the bubbling of the syrup. This increased evaporative surface causes a sharp increase
20 in the drying rate and the liquid foam dries into solid glass foam (FGM). Typically, this occurs soon after boiling.

Temperatures for the boiling step can be above or below ambient temperature. Preferably, the external temperature for the boiling step is about 5 to 80°C. More preferably, the external temperature is about 5 to 60°C; even more
25 preferably, about 5 to 35°C.

The drying process results in formation of bubbles which greatly increases the evaporative surface area of the syrup. This allows increased evaporation of residual solvent and the FGM vitrifies as a solid foam of the bubbles which result from the boiling step. The endpoint of the boiling step can be determined by an
30 increase in sample temperature, which is preferably maintained for a period of

time sufficient to ensure complete drying. The optimum time varies from sample to sample but is easily determinable by one of skill in the art.

Various container shapes and sizes can be processed simultaneously. Ideally, the container size used is sufficient to contain the initial mixture and accommodate the volume of the dried cells formed thereof. Generally, 3 ml pharmaceutical vials are used. Any such vials can be used, including Wheaton molded and tube-cut vials. Preferably, the vials are moisture resistant so as to eliminate any deleterious effects due to moisture uptake by a sample.

Residual moisture content can be measured using assays known in the art, such as Karl Fischer coulometric method and gravimetric method. For determination of residual moisture using a Coulometer, residual moisture is extracted using formamide, followed by measurement using a Coulometer. Percent moisture in the sample (w/w) is determined using the following formula:

$$\frac{\text{test sample} - \text{blank} \times 10^3 \times 10^2}{\text{wt of dried sample (mg)} \times 10^2 \times 10^3} \% \text{ residual moisture}$$

A more detailed description of this assay is provided in Example 2. Preferably, residual moisture will be equal to or less than about 5%, more preferably less than about 4%, more preferably equal to or less than about 3% even more preferably equal to or less than about 2.5%. When cells are dried more rapidly by gradually increasing the temperature, as described above, residual moisture may drop below 2%. The allowable maximum for different cell types can easily be determined empirically. Generally, residual moisture above about 5% can be detrimental to viability. This varies depending, *inter alia*, on the genus/species/strain used, the concentration and type of non-reducing carbohydrate used in the drying solution, method of drying and type of storage.

The resultant glass or FGM containing the dried, stabilized prokaryotic cells should have a T_g sufficiently high to preserve the cells. " T_g " refers to the temperature at which the glass undergoes a transition into liquid phase. Variables

that determine T_g include, but are not limited to, the amount of residual moisture of the dried preparation(s) and the type of stabilizing agent used. Generally, protein and polysaccharides raise T_g , while salts generally lower T_g . Figure 4 illustrates the relationship between T_g and percent residual moisture.

5 For purposes of this invention, T_g should be at least about 70°C, preferably at least about 75°C, more preferably at least about 80°C, even more preferably at least about 85°C, most preferably at least about 90°C. T_g can be determined using standard techniques in the art, such as differential scanning calorimetry. Generally, the higher the T_g , the higher the allowable storage temperature.

10 The length of time required to achieve the desired residual moisture and/or T_g will depend on several variables, including, but not limited to, sample size, pressure and temperature. Generally, the longer the samples are dried, the lower the residual moisture (and hence the greater the T_g). Figure 5 shows the relationship between residual moisture and length of drying time. Drying can be
15 achieved in as few as 20 hours, more generally within about 24 hours. Gradually increasing the temperature during drying, as described above, lowers the drying time without significantly reducing cell viability (Example 6).

Prokaryotic cells dried by the methods disclosed herein can be stored for varying lengths of time at ambient or higher temperatures. The length of time the
20 dried, stabilized prokaryotic cells can be stored will depend, inter alia, on the genus, species, and/or strain of the prokaryotic cell, the degree of intracellular trehalose production and/or concentration, the concentration and type of stabilizing agent in the drying solution, the drying protocol followed, the amount of residual moisture after drying, and the acceptable degree of viability.

25 *Reconstitution of stabilized cells.* The prokaryotic cells can be reconstituted after drying by adding a suitable solvent. Thus, the invention includes methods of reconstituting prokaryotic cells that have been obtained by the methods described herein. The nature and amount of solvent used for reconstitution will depend upon the prokaryotic cells as well as their intended use.
30 Such determinations can be made empirically by those skilled in the art.

Generally, cells can be reconstituted with an aqueous solvent. If the cells are to be used as a pharmaceutical, reconstitution is preferably with a sterile physiologically acceptable buffer.

If the prokaryotic cells are to be used as a vaccine, and thus as an immunogenic agent, an adjuvant can be added in an amount sufficient to enhance the immune response to the immunogen. The adjuvant can be added to the prokaryotic cells before drying, for example, cholera B toxin subunit can be dried simultaneously with *V. cholera*. Alternatively the adjuvant can be separately reconstituted along with the prokaryotic cells.

Suitable adjuvants include, but are not limited to, aluminum hydroxide, alum, QS-21 (U.S. Pat. No. 5,057,540), DHEA (U.S. Pat. Nos. 5,407,684 and 5,077,284) and its derivatives (including salts) and precursors (e.g., DHEA-S), beta-2 microglobulin (WO 91/16924), muramyl dipeptides, muramyl tripeptides (U.S. Pat. No. 5,171,568), monophosphoryl lipid A (U.S. Pat. No. 4,436,728; WO 92/16231) and its derivatives (e.g., Detox™), and BCG (U.S. Pat. No. 4,726,947). Other suitable adjuvants include, but are not limited to, aluminum salts, squalene mixtures (SAF-1), muramyl peptide, saponin derivatives, mycobacterium wall preparations, mycolic acid derivatives, nonionic block copolymer surfactants, Quil A, cholera toxin B subunit, polyphosphazene and derivatives, and immunostimulating complexes (ISCOMs) such as those described by Takahashi et al. (1990) *Nature* 344:873-875.

For veterinary use and for production of antibodies in animals, mitogenic components of Freund's adjuvant can be used. The choice of an adjuvant depends in part on the stability of the vaccine in the presence of the adjuvant, the route of administration, and the regulatory acceptability of the adjuvant, particularly when intended for human use. For instance, alum is approved by the United States Food and Drug Administration (FDA) for use as an adjuvant in humans.

Cell viability (i.e., survival) can be determined using any of a number of techniques known in the art, such as, for example, a plate assay for colony forming units (CFU). Viability can be determined at any time, including before

and immediately after the cells are dried as well as upon various times during storage. It may be desirable to test viability after reconstitution but before application and/or administration of the cells.

5 For a plate assay, cells are reconstituted at desired time(s) with a desired solvent, generally sterile distilled water of a volume at least equal to the volume of the dried cells. After vortexing, solutions of reconstituted cultures are diluted (generally 10-fold) in mineral media (for example M9 minus a carbon source) and plated in triplicate on appropriate nutrient again within 30 minutes, more preferably within 15 minutes. After incubation at 37°C for 18-24 hours, the
10 number of colony forming units (CFU) is determined. Survival is calculated as a percentage of zero time colony counts. A more detailed description of the plate viability assay is provided in Example 2.

Compositions of cells made by the methods herein. The invention also encompasses compositions comprising prokaryotic cells obtained by the methods
15 described herein. The compositions include, but are not limited to, dried prokaryotic cells and reconstituted prokaryotic cells made according to the methods described herein. The compositions may further comprise any pharmaceutically acceptable vehicle or excipient, which are well known in the art.

The following examples are provided to illustrate but not limit the
20 invention. *S. typhimurium* 1344 and *S. typhi* Ty21a were obtained from the National Institute of Biological Standards and Control, South Mimms, UK.

Example 1

Effect of osmotic shock on production of intracellular trehalose in *E. coli*

E. coli NCIMB strain 9484 was cultured in Evans medium (pH 7.0:

Table 1) containing one of a variety of agents for increasing osmotic pressure.

5 After overnight incubation at 37°C in initial Evans medium, a 4 ml culture of *E. coli* grown in Evans medium under nitrogen limitation was used to inoculate a 200 ml culture of Evans medium osmotic shock.

Table 1. Evans medium and Evans osmotic shock medium

	Initial Evans Medium	Osmotic Shock Evans medium
glucose	140 mM	10 g/l glucose
NH ₄ Cl	5 mM	3–5 g/l NH ₄ Cl (15 mM)
KCl	5 mM	0.5 M NaCl = 29.22 g/l
Na ₂ SO ₄	1.8 mM	1.8 mM
citric acid	1 mM	1 mM
MgCl ₂	0.3 mM	0.3 mM
CaCl ₂	0.5 mM	0.5 mM
NaH ₂ PO ₄	5.6 mM	5.6 mM
Na ₂ HPO ₄	20 mM	20 mM
ZnSO ₄	3.8 mM	3.8 mM
FeCl ₂	50 mM	50 mM
MnCl ₂	25 mM	25 mM
CuCl ₂	2.5 mM	2.5 mM
H ₃ BO ₃	2.5 mM	2.5 mM
CoCl ₂	0.5 mM	0.5 mM
chloramphenicol	50 mg/liter	50 mg/liter

10

Intracellular trehalose concentration was measured as described below at various times after the initiation of osmotic shock.

Determination of intracellular trehalose concentration

Intracellular concentration of trehalose was determined using high pressure liquid chromatography (HPLC) as follows. Trehalose standards were prepared by first making 10 mM trehalose in 70% ethanol, followed by 10-fold serial dilution from 10 mM to 10 nM using 70% ethanol as diluent. Thirty μ l of the standard was placed in a microtube which was placed in an 80°C water bath for 5 minutes, while noting the initial volume of the supernatant following incubation. Microtubes were centrifuged at 13,000 rpm for 10 minutes and the supernatant removed. After adding an equal volume of chloroform to the supernatant, the samples were vortexed and centrifuged at 13,000 rpm for 10 minutes. The chloroform extractions were repeated another two times. The final volume of the supernatant was adjusted to 500 μ l using deionized water. A calibration curve was generated by testing samples at varying concentrations.

Cell samples were prepared for analysis by disrupting the cell wall by sonication (any other method such as mortar and pestle, osmotic lysis, beads can be used) coupled with the preferential solubilization of trehalose in 70% ethanol, followed by removing triglycerides by chloroform extraction. One ml of cell suspension was aliquoted into a microtube, which was centrifuged at 13,000 rpm for 10 minutes. The pellet was resuspended with 100 μ l of 70% ethanol (initial volume). The pellet volume was determined by measuring the relative increase in the initial volume following resuspension of the cells. The cell suspension was incubated in a water bath at 80°C for 5 minutes. The tubes were centrifuged at 13,000 rpm for 10 minutes and the supernatant removed. An equal volume of chloroform was added and the centrifugation step repeated. Chloroform extraction was performed a total of three times. The final volume of supernatant was adjusted to 500 μ l using deionized water.

Quantitation of trehalose was achieved by HPLC (Beckman Instruments), using a Dionex CarboPac PA 100 analytical column, with a Dionex ED40 pulsed amperometric electrochemical detector. Total trehalose concentration from the original cell pellet was determined as a fraction of the final volume extracted and

the pellet volume multiplied by the trehalose concentration determined using the following formula:

$$\frac{\text{Final volume of supernatant}}{\text{Pellet volume}} \times \text{Trehalose concentration}$$

5 Final volume of supernatant was the aqueous volume remaining after the final chloroform extraction. Pellet volume was the difference in the resuspended pellet following the addition of 100 μ l of 70% ethanol. Concentration of trehalose formed was determined using the trehalose concentration curve.

10 The results obtained are shown in Figure 6. Significant increases in intracellular trehalose concentrations were observed at 15–17 hours after initiation of osmotic shock, with values peaking at less than 20 hours.

Example 2

Stabilization and reconstitution of *E. coli* using trehalose

15 *E. coli* (strain 9484) was placed in 100 ml batch cultures of a minimal medium related to M9 (minimal medium) but with high (0.5 M) salt content (Na_2HPO_4 , 6 g/l; KH_2PO_4 , 3 g/l; NH_4Cl , 0.267 g/l; NaCl, 29.22 g/l; 1 M MgSO_4 , 1 ml/l; 0.1 M CaCl_2 , 1 ml/l; thiamine HCl, 1 ml/l; glucose at final concentration of 2.5% w/v). This is "modified M9 medium." Cells were grown for 22 hours at
20 37°C with shaking. A control culture where the medium was supplemented with 20 mM betaine, in which trehalose synthesis would be markedly reduced, was also prepared. Samples of cultures were removed for trehalose determination (3 x 1 ml) as described in Example 1 and protein estimation by the Bradford assay (3 x 10 ml; Bio-Rad).

25 Two 25 ml aliquots of the test and control culture were harvested by centrifugation at 10,000 rpm for 10 minutes. Cell pellets were resuspended in 5 ml of 45% trehalose, 1.5% polyvinylpyrrolidone (Kollidon 90; BASF) or 0.1% carboxymethylcellulose (Blanoes HF; Aqualon). The suspensions were then

pooled to a total volume of 10 ml with a typical density of $4-8 \times 10^9$ bacteria/ml and 300 μ l aliquots dispensed into 3 ml pharmaceutical vials.

Bacteria were dried under vacuum without freezing in a modified FTS freeze dryer according to the following protocol: vacuum, 30 mT; initial shelf
5 temperature 40°C for 16 hours, followed by ramping to 80°C at a rate of 2.5°C per minute in increments of 2°C with a holding time of 12 minutes per increment. Foaming occurred within approximately 60 minutes of initial drying.

Residual moisture content was determined as follows. One ml of formamide was carefully dispensed into each vial containing the dried bacteria in
10 trehalose. One ml of formamide added to an empty vial served as a control. Residual moisture was extracted by mixing for 15 to 20 minutes at room temperature. For the analysis, 100 μ l of the blank (control) formamide was added to a reaction vessel using disposable needles and syringes, and the value registered by the Coulometer (Karl/Fischer) was recorded. Care was taken not to
15 introduce air into the formamide samples, as air contains water vapor. The test (and control) samples were measured in duplicate. The value determined by the Coulometer was equal to μ g of water. Test sample less blank divided by 100 is equal to μ g of water per μ l of formamide in the sample. Percent moisture in the dried sample (w/w) is:

$$\frac{\text{test sample} - \text{blank} \times 10^3 \times 10^2}{\text{wt of dried sample (mg)} \times 10^2 \times 10^3} \quad \%$$

20 Viability was determined immediately after completion and at various times during storage at 37°C using a plate assay. For the plate assay, serial 10-fold dilutions of cells were set up by using minimal medium minus a carbon source as a sterile diluent.

25 Thirty μ l of the cell suspension from the sixth dilution tube was added to each of 3 LB (Luria-Bertuni) plates, using a sterile glass spreader to spread the culture over the entire surface of the plate. The plates were incubated overnight at 37°C, and the colonies counted.

X = number of colonies $X \times 33\frac{1}{3} \times 1 \times 10^6$ dilution section CFU/ml

The results for storage at 37°C up to 45 days are shown in Figure 3. Greater than 50% viability (typically 50-80%) in the trehalose induced cells was observed in samples reconstituted immediately after drying. More significantly, no further losses in viable cell recovery were observed on storage of the dried cells, even after 45 days storage at 37°C (Figure 3.).

Example 3

Southern blot analysis to detect presence of trehalose synthase gene

DNA was prepared from *E. coli*, *S. typhimurium* 1344 (1344), and *Salmonella typhi* Ty21a (Ty21a) using standard methods. *E. coli* and *Salmonella* genomic DNA were digested with restriction endonucleases Hind III (H), EcoRI (R), or Bam HI (B), separated on a 0.8% TBE (Tris-borate electrophoresis buffer) agarose gel and blotted onto nylon filters. The filters were screened using a ^{32}P -labeled probe corresponding to the *otsA/B* region of *E. coli* that codes for the trehalose synthase genes in *E. coli*. After hybridization, the filters were washed at low stringency. Exposure of the gels to X-Ray film was overnight for *E. coli* and three days for *Salmonella* spp.

The presence of trehalose synthase genes was detected in both strains of *Salmonella* as shown in Figure 2. Fainter bands were detected when filters were washed under higher stringency conditions.

Example 4

Induction of trehalose synthesis in *Salmonella*

Salmonella typhimurium (1344) was grown overnight at 37°C in either M9 (minimal) medium with and without 0.5 M NaCl. Cells were harvested by centrifugation and analyzed for intracellular trehalose concentration by HPLC analysis as described in Example 1. The results are shown in Figure 7. Growth in high salt medium showed at 4 to 5 fold induction of trehalose synthesis.

Example 5

Relation between T_g and residual moisture

E. coli (strain 9484) were grown in M9 media containing high salt as described in Example 2. For drying, cells were suspended in an aqueous drying solution containing 45% trehalose and 1.5% Kollidon 90 and dried for 3-24 hrs under vacuum as described in Example 2. Cells were collected at various times, and the residual water content and T_g were measured on aliquots of the same sample to eliminate any possible vial-to-vial variation. The results of the relationship of T_g and residual moisture are shown in Figure 4.

Example 6

Comparison of effect of slower and faster drying on viability

E. coli (strain 9484) were grown in modified M9 media described in Example 2. For drying, cells were suspended in an aqueous drying solution containing 45% trehalose and 0.1% carboxymethyl cellulose (Blanose H.F., Aqualon).

Two different drying protocols were followed: (a) pressure, 30 mT; external temperature 40°C for 16 hours, followed by increasing (ramping) the temperature to 80°C at the rate of 0.04°C/minute in increments of 2°C, holding each increment for about 60 minutes (slow drying); (b) pressure, 30 mT; external temperature 40°C for 16 hours, followed by increasing the temperature to 80°C at the rate of 2.5°C/minute in increments of 2°C, holding each increment for about 12 minutes (fast drying).

Viability was measured immediately after drying. The samples prepared by fast drying were no less viable than those samples prepared by slow drying. Ranges between about 48% and 52% were observed for the "fast" dried samples, while between about 40% and 52% were observed for the "slow" dried samples. On average, the "fast" dried samples displayed higher viability than the "slow" dried samples.

The effect of length of drying time on viability is shown in Figure 8. The drying solution contained 45% trehalose and 0.1% CMC; the FTS drying protocol was 30 mT ST 40°C for varying times.

Example 7

Comparison of the effects of different excipients on stabilising the outer membrane of *E. coli* 9894 following intracellular induction of trehalose

E. coli strain 9894 was inoculated in 100 ml batch cultures of minimal medium related to M9 but with high (0.5M) salt content as described in Example 2. Cells were grown for 22 hours at 37°C in a shaking incubator (early stationary phase). Samples of cultures were removed for trehalose determination (3 x 1 ml) and protein estimation by the Bradford assay (3x10 ml; Bio-Rad). Trehalose concentration was expressed as $\mu\text{mol (mg protein)}^{-1}$.

Intracellular concentration of trehalose was determined using ion exchange chromatography with electrochemical detection. Calibration standards were prepared by first making a stock solution of 1 mM trehalose, glucose, sucrose and maltose standards in water, followed by serial dilutions from 1 mM to 2.5 μM using water as a diluent.

One ml of cell suspension was aliquoted into a microtube, which was centrifuged at 13,000 rpm for 10 minutes and the supernatant removed. The cell pellet was resuspended in 200 μl of 80% ethanol. The cell suspension was prepared for analysis by disrupting the cell wall in a 80°C bath for 10 minutes, coupled with preferential solubilisation of all intracellular sugars in 80% ethanol. The suspension was centrifuged and the supernatant removed. An equal volume of chloroform was added to the supernatant and vortexed, and the sample was centrifuged removing triglycerides by the chloroform extraction. The aqueous layer was transferred into a fresh Eppendorf tube and the chloroform extraction repeated. The aqueous layer was aliquotted into HPLC vials and vacuum dried, followed by rehydration using 500 μl sterile water.

Quantitation of trehalose was achieved by HPLC (Dionex DX-500), using a Dionex CarboPac PA analytical column, with a Dionex ED40 pulsed amperometric electrochemical detector. The concentration of trehalose was determined from the calibration curve.

5 Two 30 ml aliquots from each flask were harvested by centrifugation at 10,000 rpm for 10 minutes. Cell pellets were resuspended in 8 ml of 25-45% sugar, 0.1% CMC (sodium carboxymethyl cellulose; Blanose 7HF; Aqualon). The suspensions were then pooled to a total volume of 16 ml with a typical cell density of $4-8 \times 10^9$ CFU/ml and 300 μ l aliquots dispensed into 3 ml
10 pharmaceutical vials.

Bacteria were dried under vacuum without freezing using the following protocol: vacuum, 30 mT; initial shelf temperature 40°C for 16 hours, followed by ramping to 80°C at a rate of 2.5°C/min in increments of 2°C with a holding time of 12 minutes per increment. Foaming occurred between 60-120 minutes of
15 initial drying.

Viability was determined immediately before and after the completion of the drying procedure and at various times during storage at 37°C using a plate assay as described in Example 2. The residual moisture content and the glass transition temperature were also determined.

20 The results for storage at 37°C are shown in Table 2. No significant loss in viable cell recovery was observed after 6 weeks storage of *E. coli* at 37°C using the non-reducing sugars trehalose, palatinit or lactitol as excipients for stabilizing the outer membrane. More significantly, greater than 99% loss was observed for the reducing sugar glucose.

Table 2. *E. coli* 9484 viable cell recovery immediately after completion of QT4 drying and following 3 and 6 weeks storage at 37°C

% Viable Cell Recovery after storage at 37°C			
Excipient	Day 0	Week 3	Week 6
Trehalose	36	52	45
Palatinit	49	49	51
Lactitol	42	36	34
Glucose	0.8	0.1	0.05

5

Example 8

Comparison of QT4 (the method of example 2) and freeze-dried *E. coli* *E. coli* NCIMB strain 9484 was inoculated in 250 ml batch culture of modified M9 medium. The composition of this medium was described in Example 2. Cells were grown for 24 hours at 37°C in a shaking incubator until early stationary phase. Samples of cultures were removed for trehalose determination (6x1 ml) and protein estimation by the Bradford assay (5x10 ml) as described in Example 7.

Eight 25 ml aliquots were removed from the flask and the bacteria harvested by centrifugation at 10,000 rpm for 10 minutes. Cell pellets were resuspended in 8 ml of 45% trehalose, 0.1% CMC (sodium carboxymethyl cellulose; Blanose 7HF; Aqualon). The cell suspensions were then pooled to a total volume of 64 ml with a typical cell density of $0.5-1.2 \times 10^9$ CFU/ml. 300 μ l and 500 μ l aliquots were dispensed into 3 ml pharmaceutical vials for foaming and freeze-drying procedures respectively.

The bacteria were dried under vacuum without freezing using the QT4 foaming protocol as described Example 2. The bacteria were freeze-dried using the following protocol: ramp at 2.5°C/min to an initial shelf temperature of -40°C; primary drying was performed at a vacuum pressure of 30 mT at -40°C,

held for 40 hours: secondary drying was performed by a ramp at 0.05°C/min from -40 to 30°C and holding for 12 hours.

Viability was determined immediately before and after the completion of the drying procedures and after 3 weeks storage at 37°C using a plate assay as described in Example 2. The residual moisture content and the glass transition temperature were also determined.

The results for storage at 37°C are shown in Table 3. No significant loss in bacterial viability was observed after 3 weeks storage at 37°C in either the bacteria dried by the QT4 method or the freeze-dried bacteria. The residual moisture content and the glass transition temperature for the QT4-dried bacteria was 1.85±0.2% and 69.05± 5.0°C respectively. The Tg for the freeze-dried bacteria was 104.5 ±2.1°C and the residual moisture content was 0.70 ±0.2%.

Table 3. Comparison between QT4 drying and freeze drying on viable cell recovery of *E. coli* 9484 after storage at 37°C

% Viable cell recovery after storage at 37°C		
	Day 0	Week 3
QT4sys (Drying)	43.7±10.3	45.1±8.5
QT4sys (Control)	2.51±0.2	<0.01
Freeze Drying	30.6±3.6	30.1±3.7
Freeze Drying (Control)	1.83±0.6	<0.01

Example 9

Intracellular accumulation of trehalose during growth of *S. typhimurium* at 37°C in a high salt medium

S. typhimurium 1344 was grown in batch culture in either minimal Salmonella growth medium with or without 0.5M NaCl (NaCl, 29.22 g l⁻¹; (NH₄)₂SO₄, 0.66g l⁻¹; K₂HPO₄, 10.5 g l⁻¹; KH₂PO₄, 4.5g l⁻¹; MgSO₄, 0.1 g l⁻¹; tryptophan, 20 mg l⁻¹; glucose at a final concentration of 2.5% w/v) for a period

of 106 hours at 37°C. Samples were removed periodically for protein measurement by the Bradford Assay and intracellular trehalose determination by HPLC as described in Example 7. Trehalose concentrations were expressed in Tmol of trehalose (mg protein)⁻¹.

5 Significant concentrations of trehalose were observed between 30 and 76 hours after inoculation reaching a maximum of 0.53 µmol of trehalose (mg protein)⁻¹ after 48 hours as shown in Figure 9.

Example 10

10 Stabilization of *S. typhimurium* 1344 at 37°C using trehalose

S. typhimurium 1344 was grown in batch culture in minimal Salmonella growth medium with 0.5M NaCl. Cells were grown for 60 hours at 37°C in a shaking incubator and harvested by centrifugation at early stationary phase. A control culture where the basal medium contained no salt was also prepared and
15 harvested at stationary phase in which trehalose synthesis would be markedly reduced, since there is no osmotic stress.

Two 25 ml aliquots from each flask were harvested by centrifugation at 10,000 rpm for 10 minutes. Cell pellets were resuspended and washed in the appropriate growth medium. The resulting cell pellet was resuspended in 8 ml of
20 45% trehalose, 0.1% CMC (Blanose 7HF; Aqualon). The suspensions were then pooled to a total volume of 16 ml with a typical cell density of 2-4 x 10⁹ CFU/ml and 300 Tl aliquots dispensed into 3 ml pharmaceutical vials. Bacteria were dried under vacuum without freezing as described in Example 2. Foaming occurred between 60-120 minutes of initial drying.

25 Samples of cultures (3x1 ml) were removed for trehalose determination and protein estimation by the Bradford assay (3 x 10 ml; Bio-Rad). Trehalose concentration was expressed as Tmol (mg protein)⁻¹ as described in Example 7. Viability was determined immediately before and after the completion of the drying procedure and at various times during storage at 37°C using a plate assay

as described in Example 2. The residual moisture content and the glass transition temperature were also determined.

The storage results at 37°C are shown in Figure 12. No significant loss in viability was observed after 6 weeks storage in *S. typhimurium* 1344, which was osmotically induced to accumulate intracellular trehalose. Significantly, greater than 99% loss was observed for the non-induced bacteria.

Example 11

Confirmation of the presence of the trehalose-6-phosphate synthase (otsA) gene in *E. coli* (NCIMB 9484) and *Salmonella spp*

Extracted genomic DNA from *E. coli* 9484, *S. typhimurium* 1344 and *S. typhi* Ty21a were qualified by OD260/280 nm and agarose gel analysis. Each DNA preparation was prepared separately to ensure no cross-contamination. The DNA was then used to prepare PCR reactions with degenerate primers (where every third base has been substituted either with a selection of bases or an inosine to allow for any sequence changes), Guessmer primers (sequence selection based upon *Salmonella* specific codon usage) and *E. coli* primers (based purely on *E. coli* sequence) as shown in Table 4. Each set produced at least one positive reaction. The relevant fragments were run on low melting point gels and purified.

Table 4. *otsA* gene probes for *E. coli*, *S. typhimurium* 1344, and *S. typhi* Ty21a

Target DNA	<i>otsA</i> gene (fragment size/application)	Primer set used
<i>E. coli</i> 9484	700 bp/Sequence	<i>E. coli</i> based
<i>E. coli</i> 9484	150 bp/Southern Probe	<i>E. coli</i> based
<i>S. typhimurium</i> 1344	700 bp/Sequence	Guessmer (<i>Salmonella</i> codon usage)
<i>S. typhimurium</i> 1344	150 bp/Southern probe	Guessmer (<i>Salmonella</i> codon usage)
<i>S. typhi</i> Ty21a	700 bp/Sequence	Guessmer (<i>Salmonella</i> codon usage)
<i>S. typhi</i> Ty21a	400 bp/Sequence	<i>E. coli</i> based

The 700 bp fragments were ligated into pCR3.1 and then transferred into component cells and sequenced. The resulting sequence data for *otsA* showed a sequence homology of 77% between *S. typhimurium* 1344 and *E. coli* 9484. The sequence data also demonstrated that only 6 bases from a total of 715 were different between the two *Salmonella spp* strains.

Although the foregoing invention has been described in some detail by way of illustration and example for purposes of clarity and understanding, it will be apparent to those skilled in the art that certain changes and modifications may be practiced. Therefore, the description and examples should not be construed as limiting the scope of the invention, which is delineated by the appended claims.

SEQUENCE LISTING

(1) GENERAL INFORMATION:

- (i) APPLICANT: Tunnaccliffe, Alan G.
Welsh, David T.
Roser, Bruce J.
Dhaljwal, Kamaljit S.
Colaco, Camilo
- (ii) TITLE OF INVENTION: METHODS OF PRESERVING PROKARYOTIC CELLS
AND COMPOSITIONS OBTAINED THEREBY
- (iii) NUMBER OF SEQUENCES: 6
- (iv) CORRESPONDENCE ADDRESS:
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 - (E) COUNTRY: UK
 - (F) POST CODE: WC2A 3LS
- (v) COMPUTER READABLE FORM:
 - (A) MEDIUM TYPE: Floppy disk
 - (B) COMPUTER: IBM PC compatible
 - (C) OPERATING SYSTEM: PC-DOS/MS-DOS
 - (D) SOFTWARE: PatentIn Release #1.0, Version #1.30
- (vi) CURRENT APPLICATION DATA:
 - (A) APPLICATION NUMBER: US
 - (B) FILING DATE:
 - (C) CLASSIFICATION:
- (viii) ATTORNEY/AGENT INFORMATION:
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 - (B) REGISTRATION NUMBER: 40,130
 - (C) REFERENCE/DOCKET NUMBER: 26374-30017.00
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 - (C) TELEX: 706141 MRSNFOERS SFO

(2) INFORMATION FOR SEQ ID NO:1:

- (i) SEQUENCE CHARACTERISTICS:
 - (A) LENGTH: 488 amino acids
 - (B) TYPE: amino acid
 - (C) STRANDEDNESS: single
 - (D) TOPOLOGY: linear

(xi) SEQUENCE DESCRIPTION: SEQ ID NO:1:

Met	Val	Asn	Gln	Asp	Ile	Ser	Lys	Leu	Ser	Leu	Asn	Glu	Cys	Pro	Gly	1	5	10	15
Ser	Val	Ile	Val	Ile	Ser	Asn	Arg	Leu	Pro	Val	Thr	Ile	Lys	Lys	Asp	20	25	30	
Glu	Lys	Thr	Gly	Glu	Tyr	Glu	Tyr	Ser	Met	Ser	Ser	Gly	Gly	Leu	Val	35	40	45	
Thr	Ala	Leu	Gln	Gly	Leu	Lys	Lys	Ser	Thr	Thr	Phe	Gln	Trp	Tyr	Gly	50	55	60	
Trp	Pro	Gly	Leu	Glu	Val	Pro	Asp	Glu	Asp	Lys	Ala	Lys	Val	Lys	Arg	65	70	75	80
Glu	Leu	Leu	Glu	Lys	Phe	Asn	Ala	Ile	Pro	Ile	Phe	Leu	Ser	Asp	Glu	85	90	95	
Val	Ala	Asp	Leu	His	Tyr	Asn	Gly	Phe	Ser	Asn	Ser	Ile	Leu	Trp	Pro	100	105	110	
Leu	Phe	His	Tyr	His	Pro	Gly	Glu	Ile	Thr	Phe	Asp	Asp	Thr	Ala	Trp	115	120	125	
Leu	Ala	Tyr	Asn	Glu	Ala	Asn	Met	Ala	Phe	Ala	Asp	Glu	Ile	Glu	Gly	130	135	140	
Asn	Ile	Asn	Asp	Asn	Asp	Val	Val	Trp	Val	His	Asp	Tyr	His	Leu	Met	145	150	155	160
Leu	Leu	Pro	Glu	Met	Ile	Arg	Gln	Arg	Val	Ile	Ala	Lys	Lys	Leu	Lys	165	170	175	
Asn	Ile	Lys	Ile	Gly	Trp	Phe	Leu	His	Thr	Pro	Phe	Pro	Ser	Ser	Glu	180	185	190	
Ile	Tyr	Arg	Ile	Leu	Pro	Val	Arg	Gln	Glu	Ile	Leu	Lys	Gly	Val	Leu	195	200	205	
Ser	Cys	Asp	Leu	Ile	Gly	Phe	His	Thr	Tyr	Asp	Tyr	Ala	Arg	His	Phe	210	215	220	
Leu	Ser	Ala	Val	Gln	Arg	Ile	Leu	Asn	Val	Asn	Thr	Leu	Pro	Asn	Gly	225	230	235	240
Val	Glu	Phe	Asp	Gly	Arg	Phe	Val	Asn	Val	Gly	Ala	Phe	Pro	Ile	Gly	245	250	255	
Ile	Asp	Val	Glu	Thr	Phe	Thr	Glu	Gly	Leu	Lys	Gln	Asp	Ala	Val	Ile	260	265	270	

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Lys Arg Ile Lys Glu Leu Lys Glu Ser Phe Lys Gly Cys Lys Ile Ile
    275                      280                      285

Ile Gly Val Asp Arg Leu Asp Tyr Ile Lys Gly Val Pro Gln Lys Leu
    290                      295                      300

His Ala Leu Glu Val Phe Leu Gly Ala His Pro Glu Trp Ile Gly Lys
    305                      310                      315                      320

Val Val Leu Val Gln Val Ala Val Pro Ser Arg Gly Asp Val Glu Glu
                      325                      330                      335

Tyr Gln Tyr Leu Arg Ser Val Val Asn Glu Leu Val Gly Arg Ile Asn
                      340                      345                      350

Gly Gln Phe Gly Thr Ala Glu Phe Val Pro Ile His Phe Met His Arg
                      355                      360                      365

Ser Ile Pro Phe Gln Glu Leu Ile Ser Leu Tyr Ala Val Ser Asp Val
    370                      375                      380

Cys Leu Val Ser Ser Thr Arg Asp Gly Met Asn Leu Val Ser Tyr Glu
    385                      390                      395                      400

Tyr Ile Ser Cys Gln Glu Glu Lys Lys Gly Thr Leu Ile Leu Ser Glu
                      405                      410                      415

Phe Thr Gly Ala Ala Gln Ser Leu Asn Gly Ala Leu Ile Val Asn Pro
                      420                      425                      430

Trp Asn Thr Asp Asp Leu Ala Glu Ser Ile Asn Glu Ala Leu Thr Val
                      435                      440                      445

Pro Glu Glu Lys Arg Ala Ala Asn Trp Glu Lys Leu Tyr Lys Tyr Ile
    450                      455                      460

Ser Lys Tyr Thr Ser Ala Phe Trp Gly Glu Asn Phe Val His Glu Leu
    465                      470                      475                      480

Tyr Arg Leu Gly Ser Ser Asn Asn
                      485

```

(2) INFORMATION FOR SEQ ID NO:2:

(i) SEQUENCE CHARACTERISTICS:

- (A) LENGTH: 495 amino acids
- (B) TYPE: amino acid
- (C) STRANDEDNESS: single
- (D) TOPOLOGY: linear

(xi) SEQUENCE DESCRIPTION: SEQ ID NO:2:

Met	Thr	Thr	Asp	Asn	Ala	Lys	Ala	Gln	Leu	Thr	Ser	Ser	Ser	Gly	Gly	1	5	10	15
Asn	Ile	Ile	Val	Val	Ser	Asn	Arg	Leu	Pro	Val	Thr	Ile	Thr	Lys	Asn	20	25	30	
Ser	Ser	Thr	Gly	Gln	Tyr	Glu	Tyr	Ala	Met	Ser	Ser	Gly	Gly	Leu	Val	35	40	45	
Thr	Ala	Leu	Glu	Gly	Leu	Lys	Lys	Thr	Tyr	Thr	Phe	Lys	Trp	Phe	Gly	50	55	60	
Trp	Pro	Gly	Leu	Glu	Ile	Pro	Asp	Asp	Glu	Lys	Asp	Gln	Val	Arg	Lys	65	70	75	80
Asp	Leu	Leu	Glu	Lys	Phe	Asn	Ala	Val	Pro	Ile	Phe	Leu	Ser	Asp	Glu	85	90	95	
Ile	Ala	Asp	Leu	His	Tyr	Asn	Gly	Phe	Ser	Asn	Ser	Ile	Leu	Trp	Pro	100	105	110	
Leu	Phe	His	Tyr	His	Pro	Gly	Glu	Ile	Asn	Phe	Asp	Glu	Asn	Ala	Trp	115	120	125	
Leu	Ala	Tyr	Asn	Glu	Ala	Asn	Gln	Thr	Phe	Thr	Asn	Glu	Ile	Ala	Lys	130	135	140	
Thr	Met	Asn	His	Asn	Asp	Leu	Ile	Trp	Val	His	Asp	Tyr	His	Leu	Met	145	150	155	160
Leu	Val	Pro	Glu	Met	Leu	Arg	Val	Lys	Ile	His	Glu	Lys	Gln	Leu	Gln	165	170	175	
Asn	Val	Lys	Val	Gly	Trp	Phe	Leu	His	Thr	Pro	Phe	Pro	Ser	Ser	Glu	180	185	190	
Ile	Tyr	Arg	Ile	Leu	Pro	Val	Arg	Gln	Glu	Ile	Leu	Lys	Gly	Val	Leu	195	200	205	
Ser	Cys	Asp	Leu	Val	Gly	Phe	His	Thr	Tyr	Asp	Tyr	Ala	Arg	His	Phe	210	215	220	
Leu	Ser	Ser	Val	Gln	Arg	Val	Leu	Asn	Val	Asn	Thr	Leu	Pro	Asn	Gly	225	230	235	240
Val	Glu	Tyr	Gln	Gly	Arg	Phe	Val	Asn	Val	Gly	Ala	Phe	Pro	Ile	Gly	245	250	255	
Ile	Asp	Val	Asp	Lys	Phe	Thr	Asp	Gly	Leu	Lys	Lys	Glu	Ser	Val	Gln	260	265	270	

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Lys Arg Ile Gln Gln Leu Lys Glu Thr Phe Lys Gly Cys Lys Ile Ile
    275                                280                                285

Val Gly Val Asp Arg Leu Asp Tyr Ile Lys Gly Val Pro Gln Lys Leu
    290                                295                                300

His Ala Met Glu Val Phe Leu Asn Glu His Pro Glu Trp Arg Gly Lys
    305                                310                                315                                320

Val Val Leu Val Gln Val Ala Val Pro Ser Arg Gly Asp Val Glu Glu
                                325                                330                                335

Tyr Gln Tyr Leu Arg Ser Val Val Asn Glu Leu Val Gly Arg Ile Asn
                                340                                345                                350

Gly Gln Phe Gly Thr Val Glu Phe Val Pro Ile His Phe Met His Lys
                                355                                360                                365

Ser Ile Pro Phe Glu Glu Leu Ile Ser Leu Tyr Ala Val Ser Asp Val
    370                                375                                380

Cys Leu Val Ser Ser Thr Arg Asp Gly Met Asn Leu Val Ser Tyr Glu
    385                                390                                395                                400

Tyr Ile Ala Cys Gln Glu Glu Lys Lys Gly Ser Leu Ile Leu Ser Glu
                                405                                410                                415

Phe Thr Gly Ala Ala Gln Ser Leu Asn Gly Ala Ile Ile Val Asn Pro
                                420                                425                                430

Trp Asn Thr Asp Asp Leu Ser Asp Ala Ile Asn Glu Ala Leu Thr Leu
                                435                                440                                445

Pro Asp Val Lys Lys Glu Val Asn Trp Glu Lys Leu Tyr Lys Tyr Ile
    450                                455                                460

Ser Lys Tyr Thr Ser Ala Phe Trp Gly Glu Asn Phe Val His Glu Leu
    465                                470                                475                                480

Tyr Ser Thr Ser Ser Ser Ser Thr Ser Ser Ser Ala Thr Lys Asn
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```

(2) INFORMATION FOR SEQ ID NO:3:

- (i) SEQUENCE CHARACTERISTICS:
- (A) LENGTH: 517 amino acids
 - (B) TYPE: amino acid
 - (C) STRANDEDNESS: single
 - (D) TOPOLOGY: linear

(xi) SEQUENCE DESCRIPTION: SEQ ID NO:3:

Met	Pro	Ser	Leu	Glu	Asn	Pro	Thr	Phe	Gln	Asn	Glu	Ala	Arg	Leu	Leu	1	5	10	15
Leu	Val	Ser	Asn	Arg	Leu	Pro	Ile	Thr	Ile	Lys	Arg	Ser	Asp	Asp	Gly	20	25	30	
Arg	Tyr	Asp	Phe	Ser	Met	Ser	Ser	Gly	Gly	Leu	Val	Ser	Gly	Leu	Ser	35	40	45	
Gly	Leu	Ser	Lys	Ser	Thr	Thr	Phe	Gln	Trp	Tyr	Gly	Trp	Pro	Gly	Leu	50	55	60	
Glu	Val	Pro	Glu	Glu	Glu	Ile	Pro	Val	Val	Lys	Glu	Arg	Leu	Lys	Gln	65	70	75	80
Glu	Tyr	Asn	Ala	Val	Pro	Val	Phe	Ile	Asp	Asp	Glu	Leu	Ala	Asp	Arg	85	90	95	
His	Tyr	Asn	Gly	Phe	Ser	Asn	Ser	Ile	Leu	Trp	Pro	Leu	Phe	His	Tyr	100	105	110	
His	Pro	Gly	Glu	Ile	Thr	Phe	Asp	Glu	Ser	Ala	Trp	Glu	Ala	Tyr	Lys	115	120	125	
Glu	Ala	Asn	Arg	Leu	Phe	Ala	Lys	Ala	Val	Ala	Lys	Glu	Val	Gln	Asp	130	135	140	
Gly	Asp	Leu	Ile	Trp	Val	His	Asp	Tyr	His	Leu	Met	Leu	Leu	Pro	Glu	145	150	155	160
Met	Leu	Arg	Glu	Glu	Ile	Gly	Asp	Ser	Lys	Glu	Asn	Val	Lys	Ile	Gly	165	170	175	
Phe	Phe	Leu	His	Thr	Pro	Phe	Pro	Ser	Ser	Glu	Ile	Tyr	Arg	Ile	Leu	180	185	190	
Pro	Val	Arg	Asn	Glu	Leu	Leu	Leu	Gly	Val	Leu	His	Cys	Asp	Leu	Ile	195	200	205	
Gly	Phe	His	Thr	Tyr	Asp	Tyr	Thr	Arg	His	Phe	Leu	Ser	Ala	Cys	Ser	210	215	220	
Arg	Leu	Leu	Gly	Leu	Thr	Thr	Thr	Pro	Asn	Gly	Ile	Glu	Phe	Gln	Gly	225	230	235	240
Lys	Ile	Ile	Ala	Cys	Gly	Ala	Phe	Pro	Ile	Gly	Ile	Asp	Pro	Glu	Lys	245	250	255	
Phe	Glu	Glu	Gly	Leu	Lys	Lys	Glu	Lys	Val	Gln	Lys	Arg	Ile	Ala	Met	260	265	270	

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Leu Glu Gln Lys Phe Gln Gly Val Lys Leu Met Val Gly Val Asp Arg
    275                                280                                285

Leu Asp Tyr Ile Lys Gly Val Pro Gln Lys Leu His Ala Leu Glu Val
    290                                295                                300

Phe Leu Ser Asp His Pro Glu Trp Val Gly Lys Val Val Leu Val Gln
    305                                310                                315                                320

Val Ala Val Pro Ser Arg Gln Asp Val Glu Glu Tyr Gln Asn Leu Arg
                                325                                330                                335

Ala Val Val Asn Glu Leu Val Gly Arg Ile Asn Gly Lys Phe Gly Thr
                                340                                345                                350

Val Glu Phe Met Pro Ile His Phe Leu His Lys Ser Val Asn Phe Asp
    355                                360                                365

Glu Leu Ile Ala Leu Tyr Ala Val Ser Asp Ala Cys Ile Val Ser Ser
    370                                375                                380

Thr Arg Asp Gly Met Asn Leu Val Ala Tyr Glu Tyr Ile Ala Thr Gln
    385                                390                                395                                400

Lys Lys Arg His Gly Val Leu Val Leu Ser Glu Phe Ala Gly Ala Ala
                                405                                410                                415

Gln Ser Leu Asn Gly Ser Ile Ile Ile Asn Pro Trp Asn Thr Glu Glu
                                420                                425                                430

Leu Ala Gly Ala Tyr Gly Glu Ala Val Thr Met Ser Asp Glu Gln Arg
                                435                                440                                445

Ala Leu Asn Phe Ser Lys Leu Asp Lys Tyr Val Asn Lys Tyr Thr Ser
    450                                455                                460

Ala Phe Trp Gly Gln Ser Phe Val Thr Glu Leu Thr Arg Ile Ser Glu
    465                                470                                475                                480

His Ser Ala Glu Lys Phe His Ala Lys Lys Ala Ser Phe Ser Asp Asn
                                485                                490                                495

Asn Ser Glu Asn Gly Glu Pro Ser Asn Gly Val Glu Thr Pro Ala Gln
                                500                                505                                510

Glu Gln Val Ala Gln
    515

```

(2) INFORMATION FOR SEQ ID NO:4:

- (i) SEQUENCE CHARACTERISTICS:
- (A) LENGTH: 479 amino acids
 - (B) TYPE: amino acid

(C) STRANDEDNESS: single

(D) TOPOLOGY: linear

(xi) SEQUENCE DESCRIPTION: SEQ ID NO:4:

Met	Ser	Asp	Ala	His	Asp	Thr	Ile	Lys	Ser	Leu	Thr	Gly	Asp	Ala	Ser	1	5	10	15
Asn	Ser	Arg	Arg	Leu	Ile	Val	Val	Ser	Asn	Arg	Leu	Pro	Ile	Thr	Ile	20	25	30	
Lys	Arg	Lys	Asp	Asn	Gly	Thr	Tyr	Asp	Phe	Ser	Met	Ser	Ser	Gly	Gly	35	40	45	
Leu	Val	Ser	Ala	Leu	Ser	Gly	Leu	Lys	Lys	Leu	Met	Thr	Phe	Gln	Trp	50	55	60	
Leu	Gly	Trp	Cys	Gly	Gln	Glu	Ile	Pro	Glu	Asp	Glu	Lys	Pro	Met	Ile	65	70	75	80
Ile	Gln	Arg	Leu	Gln	Asp	Glu	Cys	Ser	Ala	Ile	Pro	Val	Phe	Leu	Asp	85	90	95	
Asp	Glu	Thr	Ala	Asp	Arg	His	Tyr	Asn	Gly	Phe	Ser	Asn	Ser	Ile	Leu	100	105	110	
Trp	Pro	Leu	Phe	His	Tyr	His	Pro	Gly	Glu	Ile	Asn	Phe	Asp	Glu	Glu	115	120	125	
Asn	Trp	Glu	Ala	Tyr	Arg	Ala	Ala	Asn	Tyr	Ala	Phe	Ala	Glu	Ala	Ile	130	135	140	
Val	Lys	Asn	Leu	Gln	Asp	Gly	Asp	Leu	Ile	Trp	Val	Gln	Asp	Val	His	145	150	155	160
Leu	Met	Val	Leu	Pro	Gln	Met	Leu	Arg	Glu	Leu	Ile	Gly	Asp	Lys	Phe	165	170	175	
Lys	Asp	Ile	Lys	Ile	Gly	Phe	Phe	Leu	His	Thr	Pro	Phe	Pro	Ser	Ser	180	185	190	
Glu	Ile	Tyr	Arg	Val	Leu	Pro	Val	Arg	Asn	Glu	Ile	Leu	Glu	Gly	Val	195	200	205	
Leu	Asn	Cys	Asp	Leu	Val	Gly	Phe	His	Thr	Tyr	Asp	Tyr	Ala	Arg	His	210	215	220	
Phe	Leu	Ser	Ala	Cys	Ser	Arg	Ile	Leu	Asn	Leu	Ser	Thr	Leu	Pro	Asn	225	230	235	240
Gly	Val	Glu	Tyr	Asn	Gly	Gln	Met	Val	Ser	Val	Gly	Thr	Phe	Pro	Ile	245	250	255	

Gly Ile Asp Pro Glu Lys Phe Ser Asp Ala Leu Lys Ser Asp Val Val
 260 265 270
 Lys Asp Arg Ile Arg Ser Ile Glu Arg Arg Leu Gln Gly Val Lys Val
 275 280 285
 Ile Val Gly Val Asp Arg Leu Asp Tyr Ile Lys Gly Val Pro Gln Lys
 290 295 300
 Phe His Ala Phe Glu Val Phe Leu Glu Gln Tyr Pro Glu Trp Val Gly
 305 310 315 320
 Lys Val Val Leu Val Gln Val Ala Val Pro Ser Arg Gln Asp Val Glu
 325 330 335
 Glu Tyr Gln Asn Leu Arg Ala Val Val Asn Glu Leu Val Gly Arg Ile
 340 345 350
 Asn Gly Arg Phe Gly Thr Val Glu Tyr Thr Pro Ile His Phe Leu His
 355 360 365
 Lys Ser Val Arg Phe Glu Glu Leu Val Ala Leu Tyr Asn Val Ser Asp
 370 375 380
 Val Cys Leu Ile Thr Ser Thr Arg Asp Gly Met Asn Leu Val Ser Tyr
 385 390 395 400
 Glu Tyr Ile Cys Thr Gln Gln Glu Arg His Gly Ala Leu Ile Leu Ser
 405 410 415
 Glu Phe Ala Gly Ala Ala Gln Ser Leu Asn Gly Ser Ile Val Ile Asn
 420 425 430
 Pro Trp Asn Thr Glu Glu Leu Ala Asn Ser Ile His Asp Ala Leu Thr
 435 440 445
 Met Pro Glu Lys Gln Arg Glu Ala Asn Glu Asn Lys Leu Phe Arg Tyr
 450 455 460
 Val Asn Lys Tyr Thr Ser Gln Phe Trp Gly Pro Lys Leu Cys Arg
 465 470 475

(2) INFORMATION FOR SEQ ID NO:5:

- (i) SEQUENCE CHARACTERISTICS:
- (A) LENGTH: 498 amino acids
 - (B) TYPE: amino acid
 - (C) STRANDEDNESS: single
 - (D) TOPOLOGY: linear

(xi) SEQUENCE DESCRIPTION: SEQ ID NO:5:

Met	Thr	Ser	Arg	Gly	Asn	His	Gly	Ser	Lys	Thr	Ser	Ser	Asp	Lys	His	1	5	10	15
Leu	Gly	Asp	Ser	Asp	Phe	Val	Val	Val	Ala	Asn	Arg	Leu	Pro	Val	Asp	20	25	30	
Gln	Val	Arg	Leu	Pro	Asp	Gly	Thr	Ala	Ile	Trp	Lys	Arg	Ser	Pro	Gly	35	40	45	
Gly	Leu	Val	Thr	Ala	Leu	Glu	Pro	Leu	Leu	Arg	Gln	Arg	Arg	Gly	Ala	50	55	60	
Trp	Val	Gly	Trp	Pro	Gly	Val	Ile	Asn	Asp	Asn	Val	Asp	Leu	Asp	Leu	65	70	75	80
Thr	Ile	Lys	Ser	Ile	Val	Gln	Asp	Gly	Leu	Thr	Leu	Tyr	Pro	Val	Arg	85	90	95	
Leu	Asn	Thr	His	Asp	Val	Ala	Glu	Tyr	Tyr	Glu	Gly	Phe	Ser	Asn	Ala	100	105	110	
Thr	Leu	Trp	Pro	Leu	Tyr	His	Asp	Val	Ile	Val	Lys	Pro	Ile	Tyr	His	115	120	125	
Cys	Glu	Trp	Trp	Glu	Arg	Tyr	Val	Asp	Val	Asn	Arg	Arg	Phe	Ala	Glu	130	135	140	
Thr	Thr	Ser	Arg	Thr	Ala	Ala	Tyr	Gly	Gly	Thr	Val	Trp	Val	Gln	Asp	145	150	155	160
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Leu	Thr	Ile	Gly	Phe	Phe	Leu	His	Ile	Pro	Phe	Pro	Pro	Val	Glu	Leu	180	185	190	
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Ala	Asp	Leu	Val	Gly	Phe	His	Leu	Thr	Ser	Gly	Ala	Gln	Asn	Phe	Leu	210	215	220	
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Ala Thr Arg Asp Arg Asn Val Arg Arg Arg Ala Arg Glu Ile Arg Ala
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 385 390 395 400
 Asp Gly Met Asn Leu Val Ala Lys Glu Tyr Val Ala Cys Arg Asn Asp
 405 410 415
 Leu Gly Gly Ala Leu Val Leu Ser Glu Phe Thr Gly Ala Ala Ala Glu
 420 425 430
 Leu Arg Gln Ala Tyr Leu Val Asn Pro His Asp Leu Glu Gly Val Lys
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 Asp Thr Ile Glu Ala Ala Leu Asn Gln Leu Ala Glu Glu Ala Arg Arg
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 Trp Ala Arg Ser Phe Leu Asp Ala Leu Ala Glu Ala Pro Ala Arg Asp
 485 490 495
 Ala Thr

(2) INFORMATION FOR SEQ ID NO:6:

- (i) SEQUENCE CHARACTERISTICS:
- (A) LENGTH: 473 amino acids
 - (B) TYPE: amino acid
 - (C) STRANDEDNESS: single
 - (D) TOPOLOGY: linear

(xi) SEQUENCE DESCRIPTION: SEQ ID NO:6:

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Phe	Asn	Leu	Ser	Glu	Gln	Asp	Leu	Asp	Glu	Tyr	Tyr	Asn	Gln	Phe	Ser	65	70	75	80
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Phe	Gln	Arg	Pro	Ala	Trp	Asp	Gly	Tyr	Leu	Arg	Val	Asn	Ala	Leu	Leu	100	105	110	
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Pro	Pro	Lys	Leu	Ala	Gln	Leu	Lys	Ala	Glu	Leu	Lys	Asn	Val	Gln	Asn	245	250	255	
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 305 310 315 320
 Asn Gly Lys Tyr Gly Gln Leu Gly Trp Thr Pro Leu Tyr Tyr Leu Asn
 325 330 335
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 385 390 395 400
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 Thr Met Ser Leu Ala Glu Arg Ile Ser Arg His Ala Glu Met Leu Asp
 420 425 430
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 450 455 460
 Lys Val Ala Thr Phe Pro Lys Leu Ala
 465 470

CLAIMS

We claim:

1. A method of preserving prokaryotic cells comprising the steps of:

5 a) increasing intracellular trehalose concentration in the prokaryotic cells to an amount effective to increase storage stability;

 b) mixing the prokaryotic cells obtained in step a) with a drying solution comprising a stabilizing agent; and

10 c) drying the product of step b) under conditions sufficient to produce a glass form of the stabilizing agent having less than about 5% residual moisture.

15 2. The method according to claim 1, wherein the method of increasing intracellular trehalose concentration is selected from the group consisting of culturing in an osmolarity sufficient to increase intracellular trehalose production, expressing a recombinant trehalose synthase gene or genes and introducing exogenous trehalose.

20 3. The method according to claim 2, wherein the osmolarity is at least about 350 mOsmoles -1.5 Osmoles

25 4. The method according to claim 2, wherein the osmolarity is at least about 400 mOsmoles -1 Osmole.

 5. The method according to claim 2, wherein the osmolarity is at least about 300 mOsmoles.

6. The method according to claim 2, wherein the osmolarity is at least about 500 mOsmoles.

5 7. The method according to claim 2, wherein the osmolarity is increased by adding at least one salt wherein the salt is selected from the group consisting of Na_2PO_4 , KH_2PO_4 , NH_4Cl , NaCl , MgSO_4 , CaCl_2 , thiamine HCl, or any combination thereof.

10 8. The method according to claim 1, wherein the prokaryotic cells are bacteria.

 9. The method according to claim 8, wherein the bacteria are selected from the group consisting of *Escherichia*, *Bacillus*, *Salmonella*, or *Vibrio*.

15 10. The method according to claim 1, wherein the stabilizing agent is trehalose.

 11. The method according to claim 10, wherein the intracellular
20 concentration of trehalose is at least about 100 mM.

 12. The method according to claim 1, wherein the stabilizing agent is a non-reducing carbohydrate.

25 13. The method according to claim 12, wherein the drying solution comprises at least about 25% non-reducing carbohydrate.

 14. The method according to claim 12, wherein the drying solution comprises at least about 45% non-reducing carbohydrate.

15. The method according to claim 12, wherein the non-reducing carbohydrate is selected from the group consisting of trehalose, maltitol (4-O- β -D-glucopyranosyl-D-glucitol), lactitol (4-O- β -D-galactopyranosyl-D-glucitol),
5 palatinit [a mixture of GPS (α -D-glucopyranosyl-1 \rightarrow 6-sorbitol) and GPM (α -D-glucopyranosyl-1 \rightarrow 6-mannitol)], GPS, GPM and hydrogenated maltooligosaccharides and maltooligosaccharides.

16. The method according to claim 1, wherein the drying comprises the
10 following steps:

a) evaporating the solution to obtain a syrup;

b) exposing the syrup to a pressure reduced external pressure and
15 temperature sufficient to cause boiling of the syrup; and

c) removing moisture so that residual moisture does not exceed about 5%.

17. The method according to claim 16, wherein the vacuum is initially
20 about 30 mT with an initial temperature of about 40°C.

18. The method according to claim 1, wherein step c) further comprises the steps of i) holding the temperature at about 40°C for about 16 hours; and
25 ii) raising the temperature incrementally to about 80°C at a rate of about 2.5°C per minute at increment of about 2°C, wherein each increment is of a duration of about 12 minutes.

19. The method according to claim 1, where the glass has a residual
30 moisture that does not exceed about 2.5%.

20. The method according to claim 1 wherein the glass is a foamed glass matrix.

5 21. A composition obtained according to the method of claim 1.

22. The method according to claim 21, wherein the solvent is aqueous.

10 23. The method according to claim 1, further comprising the step of: d) reconstituting the prokaryotic cells by adding a suitable solvent.

24. A method for reconstituting dried, stabilized prokaryotic cells comprising adding a suitable solvent to the dried prokaryotic cells obtained in claim 1 in an amount sufficient to attain viability.

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```

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FIG. 1

SUBSTITUTE SHEET (RULE 26)

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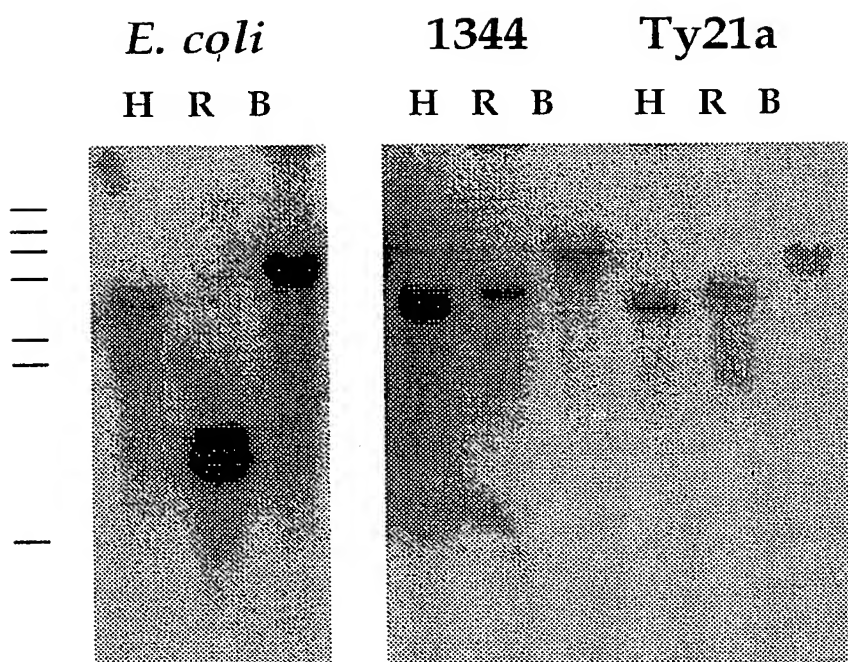


FIG. 2

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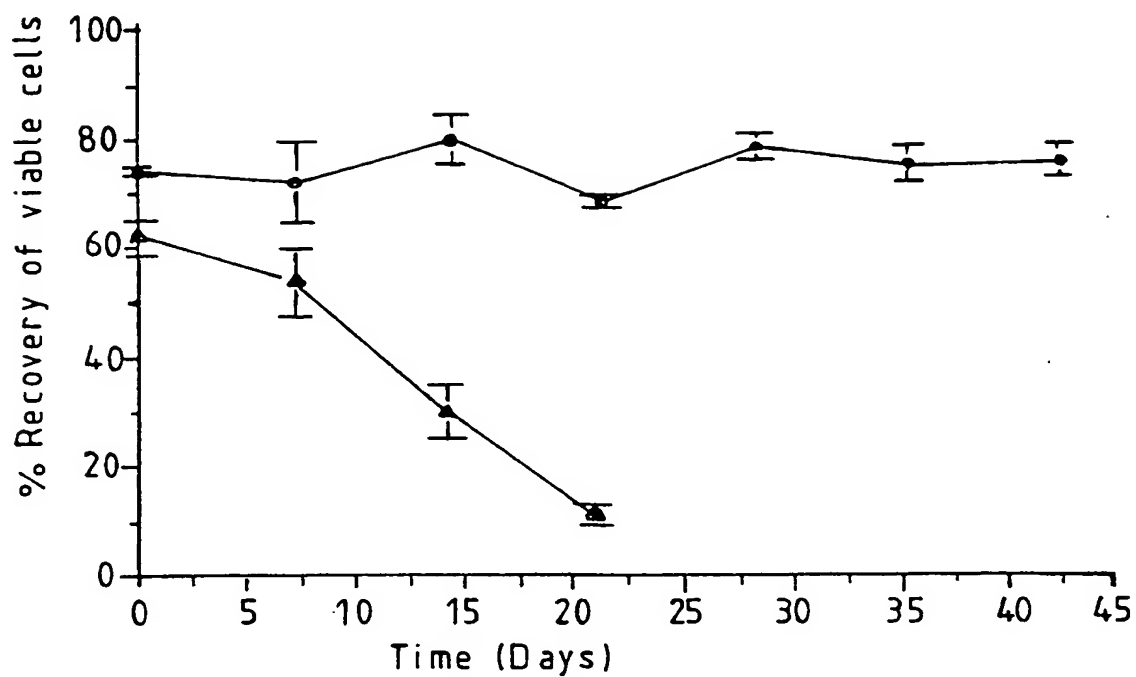


FIG. 3

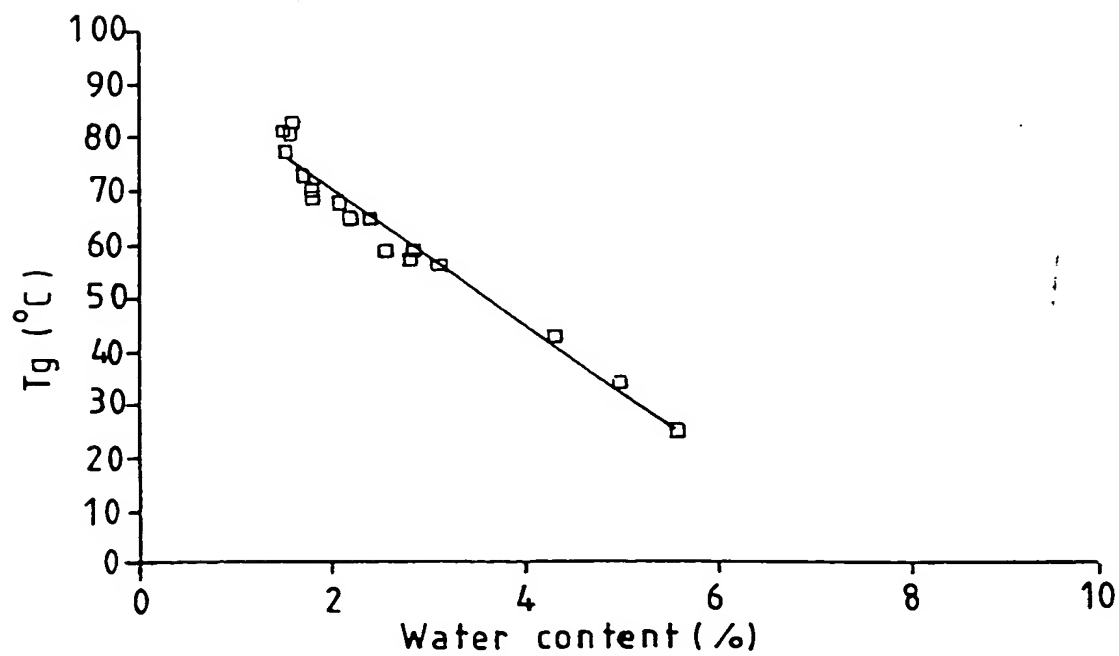


FIG. 4

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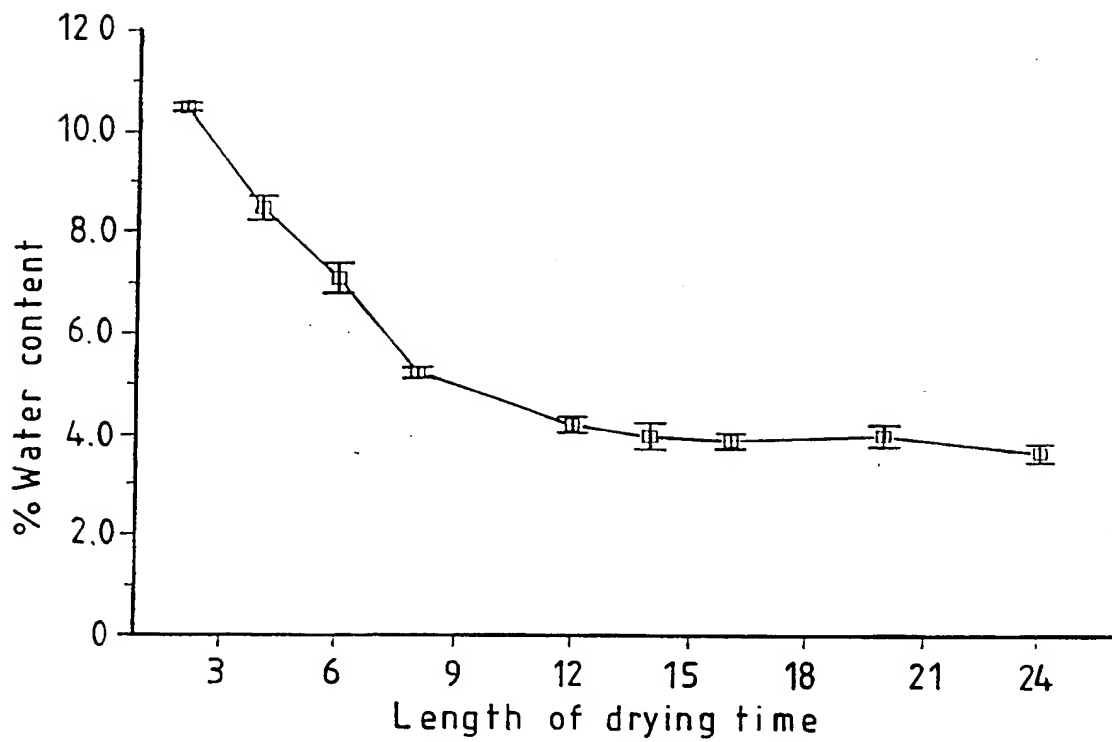


FIG. 5

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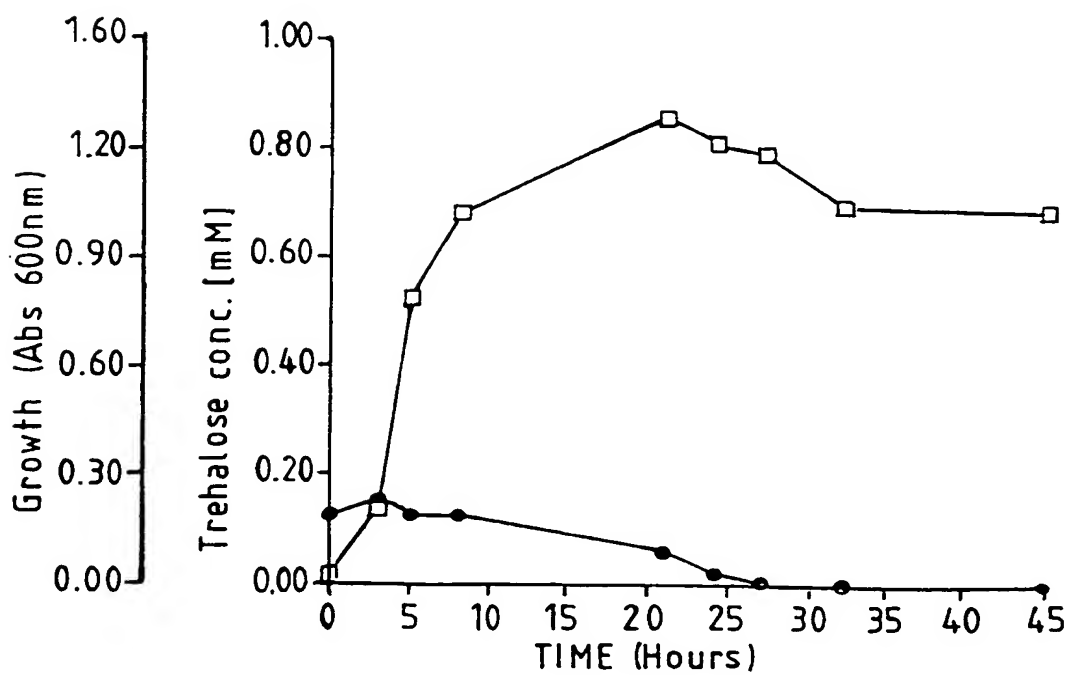
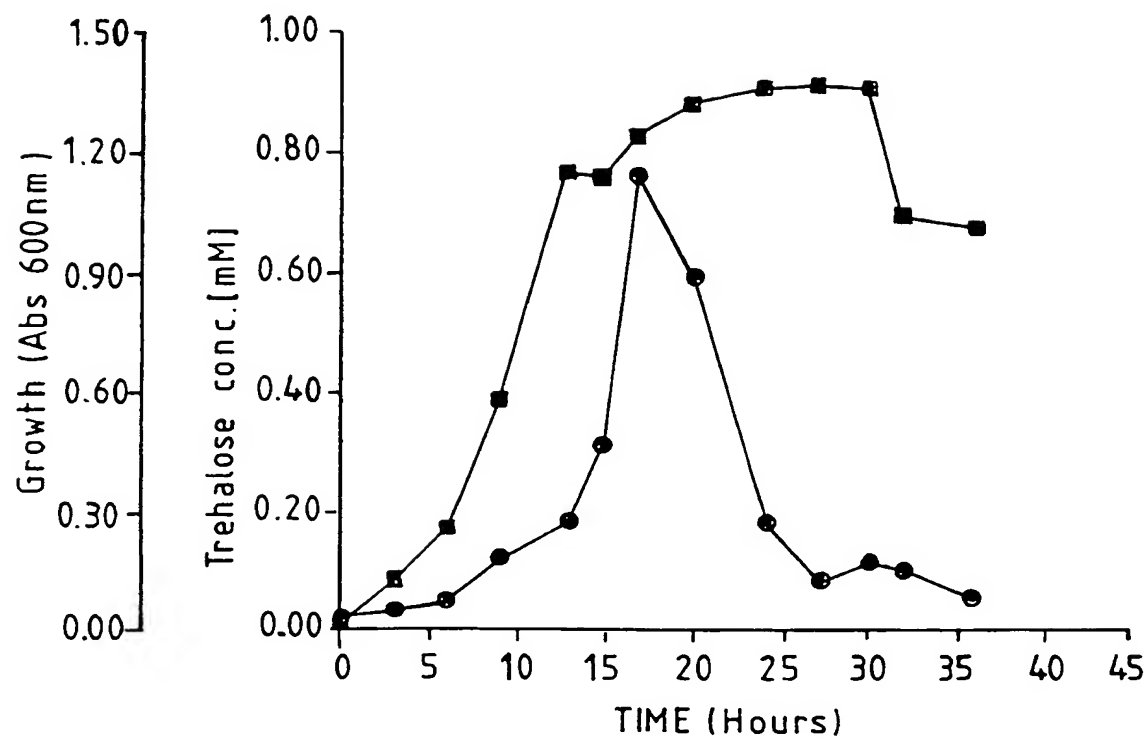


FIG. 6

SUBSTITUTE SHEET (RULE 26)

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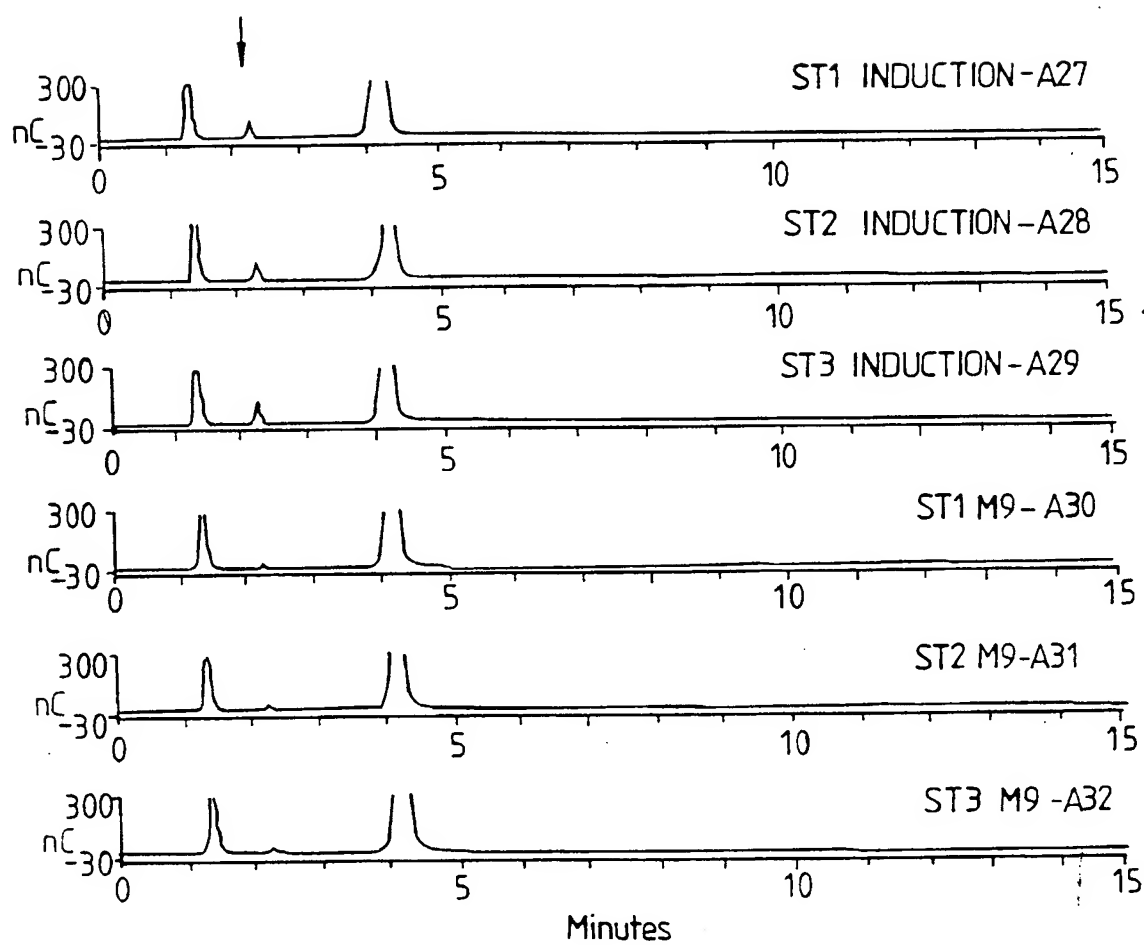


FIG. 7

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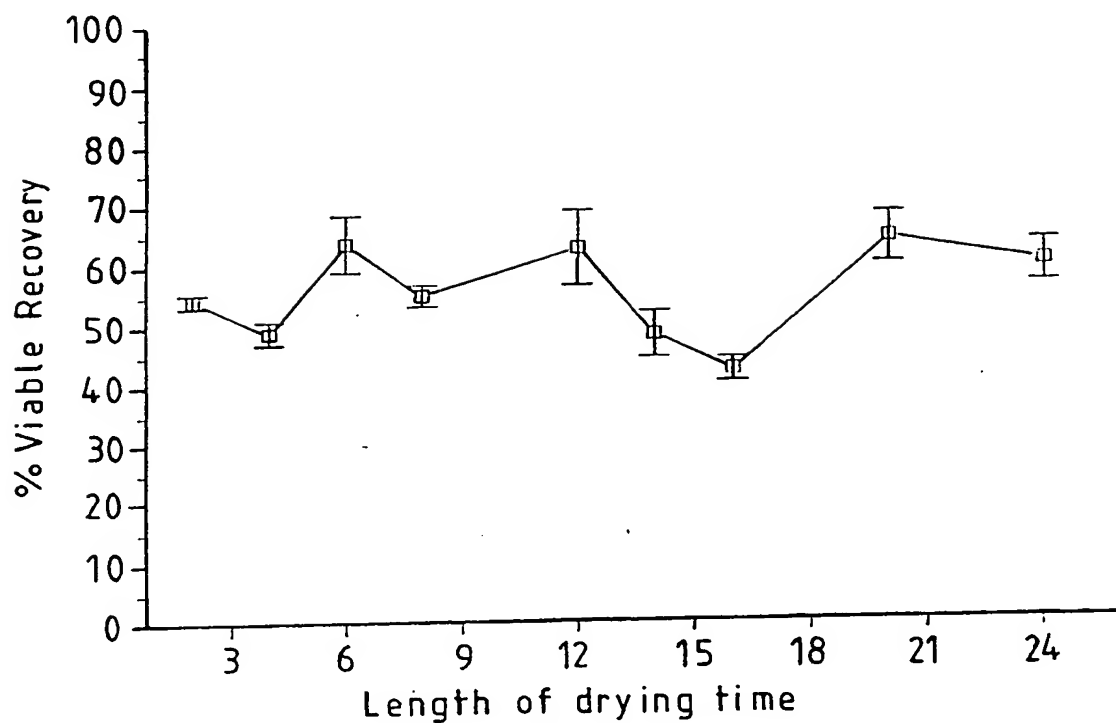


FIG. 8

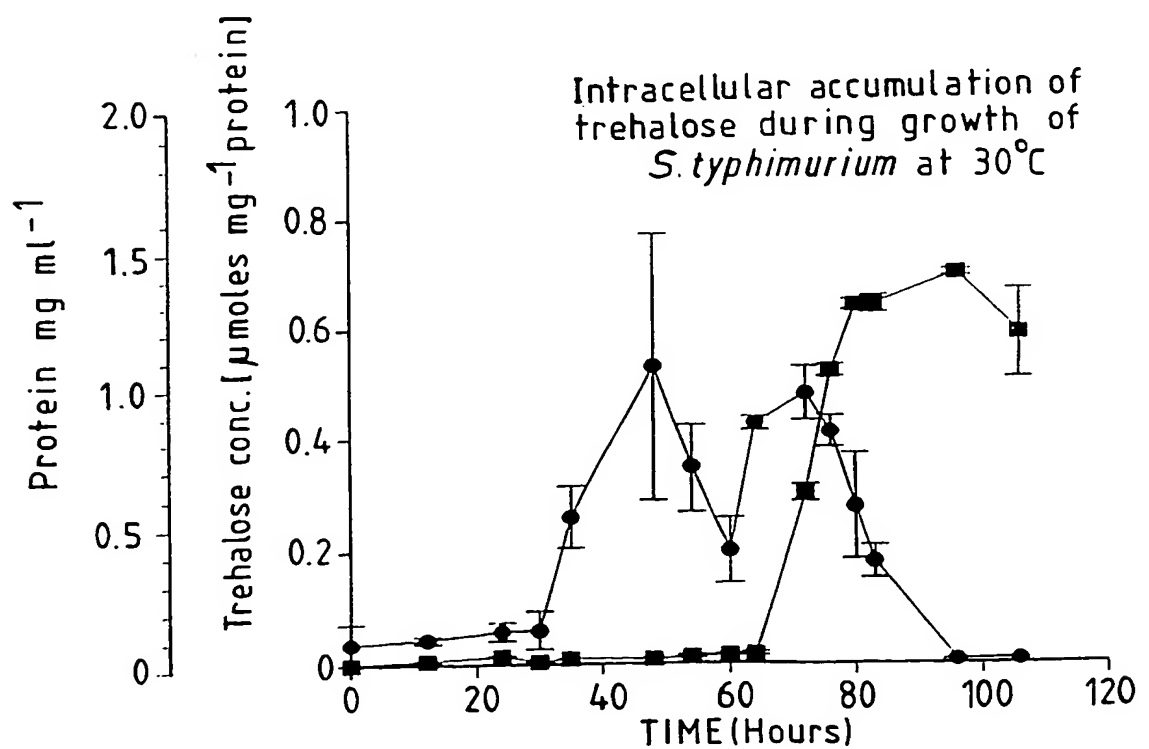


FIG. 9

● [Tre]_i
■ Protein concentration

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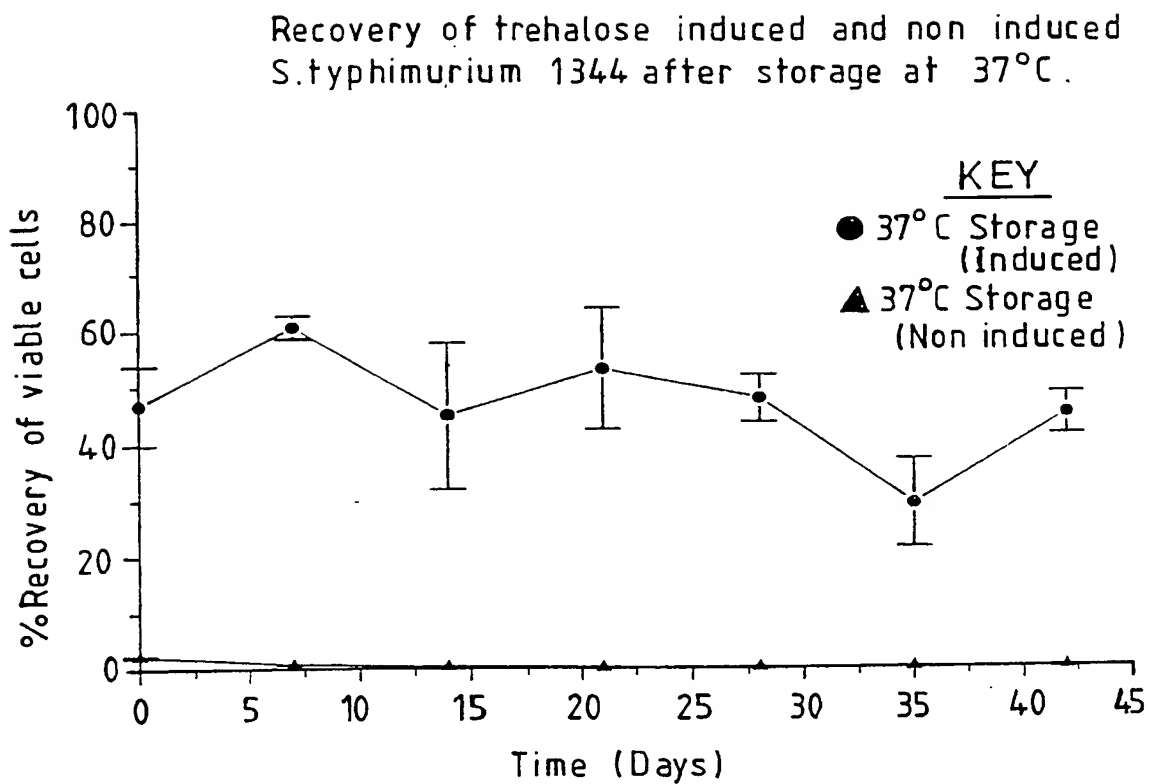


FIG. 10

INTERNATIONAL SEARCH REPORT

International Application No

PCT/GB 97/03375

A. CLASSIFICATION OF SUBJECT MATTER

IPC 6 C12N1/04 A61K35/74 A61K39/02

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 6 A61K C12N

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	P. LOUIS ET AL: "survival of Escherichia coli during drying and storage in the presence of compatible solutes" APPLIED MICROBIOLOGY AND BIOTECHNOLOGY, vol. 41, no. 6, 1994, pages 684-688, XP002059594 see page 687; figure 2	1,2, 8-15, 18, 21-24
Y	----	2-7
Y	US 5 312 909 A (DRIESSEN MARIANNE ET AL) 17 May 1994 see the whole document	2
Y	WO 95 03395 A (ZENECA LTD ;LEGG MICHAEL JEREMY (GB)) 2 February 1995 see page 2, line 1 - page 3, line 23 see page 8, line 6 - page 9, line 11 ----- -/--	2-7

☒ Further documents are listed in the continuation of box C.

☒ Patent family members are listed in annex.

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"O" document referring to an oral disclosure, use, exhibition or other means

"P" document published prior to the international filing date but later than the priority date claimed

"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.

"&" document member of the same patent family

Date of the actual completion of the international search

19 March 1998

Date of mailing of the international search report

02/04/1998

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Authorized officer

Fernandez y Branas, F

INTERNATIONAL SEARCH REPORT

International Application No

PCT/GB 97/03375

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT		
Category	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	<p>ELEUTHERIO E.C.A. ET AL: "Role of the trehalose carrier in dehydration resistance of <i>Saccharomyces cerevisiae</i>" BIOCHIMICA ET BIOPHYSICA ACTA, vol. 1156, 1993, pages 263-266, XP002059595 see front page, "Introduction"</p> <p style="text-align: center;">---</p>	1-24
A	<p>STROM A.R. ET AL: "Trehalose metabolism in <i>Escherichia coli</i>: stress protection and stress regulation of gene expression" MOLECULAR MICROBIOLOGY, vol. 8, no. 2, 1993, pages 205-210, XP002059596 see the whole document</p> <p style="text-align: center;">---</p>	1-24
A	<p>WO 93 11220 A (MASTAVAC LIMITED) 10 June 1993 see the whole document</p> <p style="text-align: center;">---</p>	1-24
A	<p>WO 96 05809 A (QUADRANT HOLDINGS CAMBRIDGE ;COLACO CAMILO (GB); ROSER BRUCE JOSEP) 29 February 1996 see the whole document</p> <p style="text-align: center;">-----</p>	1-24

INTERNATIONAL SEARCH REPORT

Information on patent family members

International Application No

PCT/GB 97/03375

Patent document cited in search report	Publication date	Patent family member(s)	Publication date
US 5312909 A	17-05-94	AT 133198 T	15-02-96
		AU 636022 B	08-04-93
		AU 7378291 A	03-10-91
		CA 2039377 A	29-09-91
		DE 69116413 D	29-02-96
		DE 69116413 T	30-05-96
		EP 0451896 A	16-10-91
		JP 5184353 A	27-07-93
		PT 97185 A	29-11-91
WO 9503395 A	02-02-95	AU 7192094 A	20-02-95
		EP 0663947 A	26-07-95
WO 9311220 A	10-06-93	AU 2954692 A	28-06-93
WO 9605809 A	29-02-96	AU 3349695 A	14-03-96
		EP 0804163 A	05-11-97

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